

One-dimensional turbulence: model formulation and application to homogeneous turbulence, shear flows, and buoyant stratified flows

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(Received 18 February 1997 and in revised form 1 March 1999)

A stochastic model, implemented as a Monte Carlo simulation, is used to compute statistical properties of velocity and scalar fields in stationary and decaying homogeneous turbulence, shear flow, and various buoyant stratified flows. Turbulent advection is represented by a random sequence of maps applied to a one-dimensional computational domain. Profiles of advected scalars and of one velocity component evolve on this domain. The rate expression governing the mapping sequence reflects turbulence production mechanisms. Viscous effects are implemented concurrently.

Various flows of interest are simulated by applying appropriate initial and boundary conditions to the velocity profile. Simulated flow microstructure reproduces the $-\frac{5}{3}$ power-law scaling of the inertial-range energy spectrum and the dissipation-range spectral collapse based on the Kolmogorov microscale. Diverse behaviours of constant-density shear flows and buoyant stratified flows are reproduced, in some instances suggesting new interpretations of observed phenomena. Collectively, the results demonstrate that a variety of turbulent flow phenomena can be captured in a concise representation of the interplay of advection, molecular transport, and buoyant forcing.

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1. Introduction

One-dimensional models of turbulent flows have been introduced in various contexts. Eddy-diffusivity formulations are often used to model ensemble-averaged flow structure in one direction, typically the vertical direction in buoyant stratified flows. One-dimensional representations of the evolution of individual flow realizations have also been formulated, such as the randomly forced Burgers equation (Chekhlov & Yakhot 1995), a one-dimensional Biot-Savart formulation (Constantin, Lax & Majda 1985; De Gregorio 1990), and one-dimensional binary-tree formulations (Aurell, Dormy & Frick 1997; Benzi *et al.* 1997).

Here, a one-dimensional simulation of individual flow realizations, denoted ‘one-dimensional turbulence’ (ODT), is formulated whose distinctive feature is the representation of turbulent advection by a postulated stochastic process rather than an evolution equation. Viscosity is incorporated as a concurrent deterministic process, governed by an evolution equation of conventional form.

In ODT, turbulent advection is represented by a random sequence of eddy motions. Each eddy motion is an instantaneous mapping of a segment of the one-dimensional domain onto itself. The eddy size (i.e. the size of the affected segment) and the time and location of its occurrence are chosen according to a random process reflecting kinetic-energy production mechanisms.

The one-dimensional domain represents a transverse direction in planar coordinates. (Implementation in cylindrical coordinates is feasible, but is not considered here.) For turbulent flows that develop temporally, flow evolution is represented by the time evolution of a streamwise velocity profile on the one-dimensional domain. For spatially developing flows, simulated flow evolution represents streamwise spatial development.

The streamwise velocity profile has two roles: it represents the strain field that generates eddy motions, and it is the observable whose statistics are compared to experimental results. Kinematical aspects of advection are represented in two dimensions, though the computational domain is one-dimensional. The eddies induce motion along the one-dimensional coordinate, while the observable corresponds to streamwise flow, perpendicular to the one-dimensional coordinate. Thus, the Reynolds stress profile $\langle u'v' \rangle$ can be obtained, despite the lack of an explicit v profile, by monitoring the transverse flux of u induced by eddy motions.

The model incorporates viscosity as well as advection. Viscous evolution is implemented by solving the appropriate transport equation for the velocity field on the one-dimensional domain. This evolution is nominally a continuous-time process, though time discretization is required for numerical implementation. This continuous evolution is punctuated by the instantaneous mapping events representing eddies. The concurrent viscous and advective processes are interactive because each process modifies the velocity field that governs both processes. Computationally affordable

resolution of viscous scales in fully developed turbulence is a key attribute of the one-dimensional formulation.

Resolution of molecular transport scales allows inclusion of diffusive scalars with no additional approximations, facilitating application of the model to turbulent dispersion, heat transfer, chemically reacting flows, etc. Scalar mixing processes that are sensitive to fine-scale turbulent motions motivated the author's earlier development (Kerstein 1991) of the linear-eddy model (LEM). That model likewise involves fully resolved molecular transport of scalars on a one-dimensional domain, concurrent with a random sequence of events representing turbulent eddies. In the LEM, flow properties are specified empirically by assigning parameters governing the random event sequence. There is no provision for feedback of local flow properties to the random process governing subsequent events.

In contrast, ODT is formulated so as to capture this feedback with minimal empiricism. In this regard, ODT is both a turbulence model and a methodology for fully resolved simulation of mixing, chemical reaction, and related scalar processes in turbulence. The latter capability is a key feature distinguishing ODT from conventional turbulence models that require the incorporation of mixing submodels in order to treat scalar processes.

Because ODT subsumes many of the previously demonstrated capabilities of the LEM with regard to mixing, the emphasis here is on flow properties. It is noted that comparable or superior predictions of particular flow properties may be obtained using conventional models. The distinguishing features of ODT are its scope, simplicity, minimal empiricism, and capability to incorporate complex molecular processes (variable transport properties, chemical reactions, dynamically active scalars, etc.) without introducing additional approximations.

Because ODT is a fully resolved simulation, various statistical quantities can be extracted that are not provided by conventional closure methods, such as single-point and multipoint moments of any order, multivariate probability density functions, conditional statistics, power spectra, level-crossing statistics, Lagrangian statistics, and fractal dimensions. Only a limited exploration of these possibilities is attempted here.

A one-dimensional formulation is applicable only to flows that are homogeneous in at least one spatial coordinate. Many flows of fundamental interest and practical importance are of this type. For more complex flows, a one-dimensional unsteady simulation may prove advantageous as a subgrid model within a large-eddy simulation or a multidimensional steady-state model. Implementation of the LEM in this manner has been demonstrated (Menon & Calhoun 1996).

The model is formulated in §2. Additional details, including numerical implementation issues, are discussed in Appendix A. Relationships between model quantities and three-dimensional flow properties are examined in Appendices B and C.

The remainder of the paper addresses various applications, which indicate the diversity of flow configurations and phenomena that can be treated. Many of the computed behaviours are direct consequences of the formulation, but in several instances new insights are gained concerning phenomena that are not yet well understood.

2. Model formulation

2.1. Overview

Operationally, ODT is a numerical method for generating realizations of a class of stochastic initial-boundary-value problems on a one-dimensional domain. For

temporal flows (T-flows), each ODT realization represents a time history, $u(y, t)$, of the transverse profile of streamwise velocity, and/or time histories of one or more scalar profiles, generically denoted $\theta(y, t)$. For spatially developing flows (S-flows), ODT generates realizations parameterized by (y, x) instead of (y, t) , where x is the streamwise coordinate. (Here, the y -coordinate is normal to the streamwise and spanwise directions.)

It is convenient to describe ODT with reference to T-flow, later explaining distinct features of the S-flow formulation. Eddy motions are governed by the strain field as characterized by variations of the instantaneous streamwise velocity $u(y, t)$ along the y -coordinate, and by analogous variations of the instantaneous buoyancy profile. For three-dimensional continuum flow, the link between these turbulence production mechanisms and the induced motions is the Navier–Stokes equation, which governs viscous as well as advective flow evolution. In ODT, the production mechanisms, the induced motions, and viscous transport are distinct entities. The time evolution of $u(y, t)$ is governed by viscous transport, whose continuum evolution is analogous to Navier–Stokes viscous transport, and a concurrent advection process consisting of a stochastic sequence of mappings applied to the one-dimensional domain. Likewise, each scalar profile is subject to molecular-diffusive transport based on the appropriate diffusion coefficient, and the same mapping sequence that is applied to $u(y, t)$. The mapping rule and the rate expression that govern the stochastic event sequence are discussed in §2.2, and viscous evolution is discussed in §2.3.

2.2. Advection

2.2.1. The one-dimensional eddy

In ODT, each eddy is an instantaneous event. Having no time duration, it has no opportunity to interact directly with other eddies. Rather, the interaction is indirect, mediated by the velocity profile $u(y, t)$ and/or profiles of dynamically active scalars such as the density $\rho(y, t)$ in buoyant stratified flow. For clarity, consideration of variable-density flow is deferred until §2.4.

An individual event is a mapping that determines a new streamwise velocity profile $\hat{u}(y)$ as a function of a given profile $u(y)$. (Here and subsequently, the argument t is suppressed where the meaning is clear.) The velocity profile is deemed to be unaffected outside a selected interval $y_0 \leq y \leq y_0 + l$, where l represents the eddy size. Thus, $\hat{u}(y) = u(y)$ for y outside $[y_0, y_0 + l]$.

To specify the functional dependence in $[y_0, y_0 + l]$, it is useful to adopt a Lagrangian viewpoint with respect to the y -coordinate. In this context, the effect of an eddy on $u(y)$ involves two mechanisms: transverse displacement of fluid elements and modification of the streamwise velocity within fluid elements.

Taking the one-dimensional domain to be a closed system, incompressibility constrains the transverse displacements associated with the eddy to be a measure-preserving map of the domain onto itself. Namely, the displacements can be represented by a mapping $\hat{y}(y)$ such that $\int_{\hat{S}} d\hat{y} = \int_S dy$, where S is any subset of the y domain and \hat{S} is the image of S on \hat{y} .

It is desirable for the inverse mapping $y(\hat{y})$ to be a continuous function of \hat{y} . This property ensures that two fluid elements that are close to each other after the mapping were close to each other prior to the mapping, thus preventing the introduction of discontinuities into the velocity profile.

Because the map $\hat{y}(y)$ is required to be measure-preserving, all velocity moments $\int u^n(y) dy$ are preserved by the map. (This property is analogous to the constancy of

area-integrated vorticity moments in incompressible two-dimensional Euler flow.) In particular, the total streamwise momentum ($n = 1$) and energy ($n = 2$) are preserved. (For S-flow, u and u^2 are volume flux and momentum flux, respectively.)

Streamwise momentum and energy conservation (volume-flux and momentum-flux conservation for S-flow) are essential properties, but the higher streamwise invariants are artifacts. An additional artifact is that energy conservation is here enforced on a particular velocity component.

These constraints do not arise in three-dimensional flow owing to the second eddy mechanism: modification of the streamwise velocity within fluid elements. Namely, the pressure-gradient term of the Navier–Stokes equation modifies velocity components and thus the orientation of the velocity vector, inducing energy redistribution among velocity components.

Here, this mechanism is omitted. This simplification necessarily fails for flows in which imposed pressure gradients drastically alter the flow structure, such as separating boundary layers. Even in the absence of imposed pressure gradients, pressure fluctuations can have important effects whose omission may have an impact on the performance of the model.

The ODT representation of an eddy is thus a mapping rule $\hat{y}(y)$ that reflects only one of two mechanisms of $u(y)$ modification by an eddy. Moreover, the mechanism that is represented is purely kinematical. However, aspects of turbulence energetics are incorporated into the rule that determines the stochastic sequence of mapping events (§2.4.1).

An important consequence of the proposed eddy representation is that the effect of an eddy on $u(y)$ is the same as on a passively advected scalar profile. If $Pr = 1$ and the scalar and streamwise velocity have the same initial and boundary conditions, then the scalar and velocity profiles evolve identically. In effect, the Reynolds analogy is exact in ODT for $Pr = 1$. This implies $Pr_T = 1$, where Pr_T is the turbulent Prandtl number. Measured values of Pr_T typically differ from unity by about 10 or 20%, lending some preliminary support to the kinematical approach.

Monin & Yaglom (1971) note that mixing-length theories likewise formulate the transfer of momentum as the transfer of a passive scalar, neglecting pressure-induced momentum changes within fluid elements. This consideration led Taylor (1932) to formulate a vorticity transfer theory based on the proposition that vorticity is transported more nearly as a passive scalar than is momentum. This proposition is based on the exact analogy between vorticity and passive-scalar transport in two-dimensional inviscid flow. In three dimensions, the analogy is less justified, so a vorticity formulation is not necessarily advantageous (Monin & Yaglom 1971). A velocity rather than a vorticity formulation is adopted in ODT, owing to its simplicity and ease of interpretation.

The mapping rule $\hat{y}(y)$ that is adopted is the ‘triplet map’ employed in the LEM (Kerstein 1991). The rule is stated here in a more general form, although only the particular form defined previously is implemented. In $[y_0, y_0 + l]$, \hat{y} is taken to be a three-valued function of y , as follows:

$$\hat{y} = \begin{cases} y_0 + f_1(y - y_0) \\ y_0 + f_2l - (f_2 - f_1)(y - y_0) \\ y_0 + f_2l + (1 - f_2)(y - y_0). \end{cases} \quad (2.1)$$

Equation (2.1) maps the interval $[y_0, y_0 + l]$ onto each of three subintervals $[y_0, y_0 + f_1l]$, $[y_0 + f_1l, y_0 + f_2l]$ and $[y_0 + f_2l, y_0 + l]$, where $0 < f_1 < f_2 < 1$.

As in LEM applications, the choice $f_1 = \frac{1}{3}$, $f_2 = \frac{2}{3}$ is implemented in all cases.

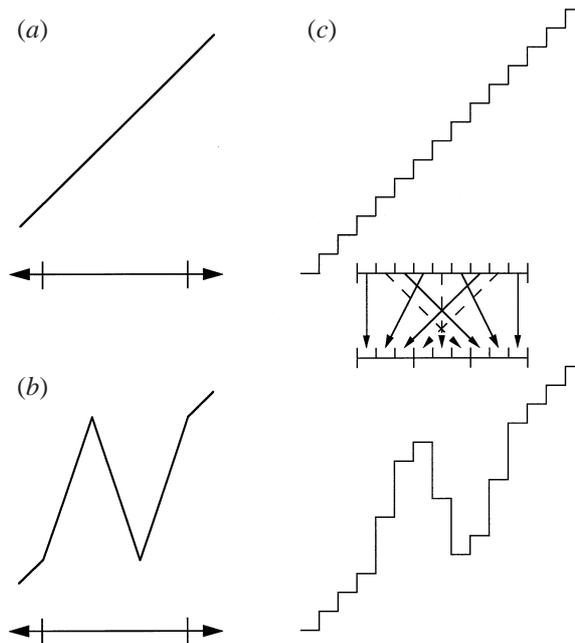


FIGURE 1. Effect of the triplet map on an initially linear velocity profile $u(y,t)$. (a) Initial profile. (b) Velocity profile after applying the triplet map to the interval denoted by ticks. (c) Discrete representation of the initial profile, and illustration of the effect of a triplet map on an interval consisting of nine cells. For clarity, arrows indicating formation of the central of the three images of the original interval are dashed.

For this choice, figure 1 illustrates the effect on a linear profile $u(y) \sim y$. The effect is to replace the profile in $[y_0, y_0 + l]$ by three compressed images of the original, with the middle image inverted (flipped). This map reflects the compressive and rotational attributes of eddy motion, as discussed in detail previously (Kerstein 1991). It causes multiplicative increase of strain intensity and a corresponding multiplicative decrease of strain length-scale. As discussed in § 3.1, these features lead to a self-similar eddy cascade.

The choice $f_1 = \frac{1}{3}$, $f_2 = \frac{2}{3}$ is simplest because it gives uniform strain intensity multiplication and length-scale reduction within the eddy. Other choices would introduce spatial variation of these properties within the eddy, governed by two empirical parameters (or one if the symmetry $f_1 = 1 - f_2$ is imposed). Allowing this empiricism might be beneficial in some contexts. For example, $f_1 = 1 - f_2 \ll 1$ would represent a mildly compressive rotation in between thin high-compression zones. This might increase the intermittency of the eddy cascade, and in the context of buoyant stratified flow, might represent convective structures that overturn with little length-scale reduction except in the high-strain regions on their periphery.

Although (2.1) is nominally a three-valued mapping, it can be approximated on a discretized computational domain by a single-valued mapping that is simply a permutation of the cells within the mapping interval $[y_0, y_0 + l]$, and thus is measure-preserving. The permutation rule, stated in its general form in Kerstein (1991), is illustrated for a particular case in figure 1(c).

That figure illustrates the continuity of the inverse mapping, as follows. Fluid elements that are nearest neighbours in the transformed profile are no more than

three cells apart in the preimage. In contrast, nearest neighbours in the preimage can be separated by more than half the eddy size in the transformed profile. This distinction is minor for the nine-cell discretization illustrated in the figure, but becomes increasingly significant as spatial resolution is improved. By considering the limit of vanishing cell size, it can be shown formally that the inverse mapping is continuous but that the forward mapping is discontinuous almost everywhere within the mapping interval $[y_0, y_0 + l]$.

2.2.2. Eddy rate distribution

As in the LEM, mapping events are governed by an ‘eddy rate distribution’ $\lambda(l)$, where $\lambda(l) dl$ is the frequency of events in the size range $[l, l + dl]$ per unit length along the y -coordinate. Based on this definition, $\lambda(l)$ has units $(\text{length}^2 \times \text{time})^{-1}$. The dimensional relation

$$\lambda(l) = 1/[l^2\tau(l)] \tag{2.2}$$

expresses $\lambda(l)$ in terms of a time $\tau(l)$ that is interpreted as an eddy time scale. A free parameter, to be determined empirically, could be inserted in (2.2). This is not done here because the principal objective here is to address qualitative behaviours with minimal empiricism. For reasons explained shortly, a free parameter is included in the expression for τ .

In the LEM, $\tau(l)$ is taken to be a mean time scale estimated by invoking the usual turbulence phenomenology. Here, this picture is modified by treating $\tau(l)$ as a local, instantaneous time scale, now denoted $\tau(l; y, t)$, whose evaluation is based on $u(y, t)$.

Dimensional reasoning suggests that $\tau(l; y, t)$ is determined by the local strain $du(y, t)/dy$, as discussed in §2.1. A refinement of this proposal that accounts for the finite spatial extent of an eddy is motivated by a Fourier picture corresponding to the parameterization $k = 1/l$. Viewing individual eddies as Fourier wave packets (Tennekes 1976), the eddy time scale can be expressed in the form $\tau_k(y, t) \sim 1/[ku_k(y, t)]$. Here, $ku_k(y, t)$ is a Fourier-space representation of $du_l(y, t)/dy$, where u_l is a smoothed u profile with smoothing scale l . This suggests the formulation

$$\tau(l; y_0, t) = \frac{l}{A\Delta u(y_0, l)}, \tag{2.3}$$

where $\Delta u(y_0, l)$ represents the velocity difference across $[y_0, y_0 + l]$ based on the smoothed velocity profile $u_l(y, t)$, and A is a free parameter. Eddy location and size are parameterized by y_0 and l , defined as in §2.2.1.

There is no uniquely preferable mathematical definition of $\Delta u(y_0, l)$. The formulation that is adopted here is

$$\Delta u(y_0, l) = 2|u_l(y_0 + \frac{1}{2}l, t) - u_l(y_0, t)|, \tag{2.4}$$

where

$$u_l(y, t) = \frac{2}{l} \int_y^{y+(l/2)} u(y', t) dy'. \tag{2.5}$$

Because numerical results may be sensitive to the functional form assumed for $\Delta u(y_0, l)$, a free parameter A has been introduced in (2.3). A is determined either empirically or by applying a self-consistency condition to the model, as appropriate for each application.

Substitution of (2.3) into (2.2) gives

$$\lambda(l; y_0, t) = 2A|u_l(y_0, t) - u_l(y_0 + \frac{1}{2}l, t)|/l^3. \tag{2.6}$$

This formulation has been motivated without reference to random fluctuations, and in fact, could be the basis of a purely deterministic model. To proceed further, it is useful to form the event rate $R(t) = \iint \lambda(l; y_0, t) dl dy_0$, where the integrations extend over the allowed ranges of the arguments. Here, two statistical hypotheses (the only such hypotheses in ODT) are introduced. First, the time sequence of mapping events is assumed to be a Poisson process whose rate at time t is $R(t)$. Second, the values (l, y_0) associated with an event occurring at time t are assumed to be randomly sampled from $\lambda(l; y_0, t)/R(t)$, which in this context is the joint probability density function (p.d.f.) of l and y_0 at time t . These assumptions define a marked Poisson process (Snyder 1975).

Though the values (y_0, l) are determined for each event by independent sampling from $\lambda(l; y_0, t)/R(t)$, values of (y_0, l) for sequential events are correlated through the effect of each event on $u(y, t)$ and thus on the functional form of $\lambda(l; y_0, t)$ that governs subsequent events. $\lambda(l; y_0, t)$ also evolves continuously in time owing to viscous evolution of $u(y, t)$. The unsteadiness of the eddy rate distribution is both a fundamental property of the model and a key consideration in its numerical implementation. Implementation is discussed in Appendix A. There it is noted that the Poisson event sequence introduces a large-scale anomaly. A large-eddy suppression mechanism that removes the anomaly in the class of flows that is most strongly affected is therefore introduced, as explained in Appendix A.

Time correlation of events introduced through the time evolution of $\lambda(l; y_0, t)$ is the mechanism that induces an eddy cascade in ODT (§3.1). However, this mechanism does not reflect the simultaneity of multiple eddies at a given spatial location, and therefore omits eddy interactions such as the sweeping of small eddies by large eddies.

This omission might be mitigated to some extent by delaying the implementation of each designated mapping by a time interval equal to the eddy time scale τ , thereby recognizing the distinction between the inception and the completion of an eddy motion. At the moment of completion, τ can be recomputed based on the updated velocity profile, and the implementation can be further delayed if the new τ value exceeds the original value.

This procedure would enhance the spatio-temporal interaction among eddies. It is not implemented, however, because the lack of finite eddy duration intrinsically limits the realism of the model in this regard. In contrast, one-dimensional binary-tree formulations (Aurell *et al.* 1997; Benzi *et al.* 1997) incorporate finite-time interactions among multiple modes, and hence a fuller representation of eddy simultaneity. It should be noted that the ultrametric spatial structure of binary-tree models precludes their application to inhomogeneous turbulence.

It is not obvious that a representation of eddy simultaneity is essential to capture the eddy-cascade observables of interest. ODT performance in this regard will be compared elsewhere to the performance of binary-tree models.

2.3. Viscosity

2.3.1. Viscous evolution equation

Viscous effects are implemented in two ways, involving a continuous-time evolution equation and a rule that suppresses certain mapping events. The latter mechanism is discussed in §2.3.2.

Continuous-time viscous evolution in the model is implemented as the one-dimensional analogue of three-dimensional viscous processes. For T-flow, it is gov-

erned by the evolution equation

$$u_t = \nu u_{yy} - P_x/\rho, \quad (2.7)$$

where ν is the kinematic viscosity, P_x is an applied pressure gradient, and ρ is the fluid density. Here, P_x can depend on t but not on x because streamwise variations are not represented within the T-flow formulation. (Time-developing channel-flow simulations with constant P_x have been implemented, but are not reported here.) Likewise, each scalar θ is subject to molecular transport governed by

$$\theta_t = \kappa \theta_{yy}, \quad (2.8)$$

where κ is the molecular diffusivity. Here, ν and κ are taken to be constants. This formulation is readily generalized to allow variable transport coefficients, non-Fickian molecular transport, and multiple, chemically reacting scalars. These generalizations have been implemented but are not reported here.

S-flows are treated in the boundary-layer approximation. The governing equations are the momentum equation

$$uu_x + \nu u_y = \nu u_{yy} - P_x/\rho, \quad (2.9)$$

the continuity equation

$$u_x + v_y = 0, \quad (2.10)$$

and the scalar transport equation

$$u\theta_x + v\theta_y = \kappa \theta_{yy}. \quad (2.11)$$

Equations (2.9)–(2.11) can be incorporated as written into ODT although ODT has no v profile. The reason is that v can be eliminated from these equations, except for its value at one reference location. This is demonstrated by using continuity to replace u_x by $-v_y$ in (2.9), formally solving (2.9) for v , and substituting this solution into (2.10) to obtain

$$u_x = -\frac{v(\hat{y})}{u(\hat{y})}u_y + v \frac{u_{yy}}{u} - \frac{P_x}{\rho u} + u_y \int_{\hat{y}}^y \frac{dy'}{u^2} \left(\nu u_{yy} - \frac{P_x}{\rho} \right), \quad (2.12)$$

where \hat{y} is a reference location. The expression for the v profile determined from (2.9) and (2.10) is

$$v = \frac{v(\hat{y})}{u(\hat{y})}u - u \int_{\hat{y}}^y \frac{dy'}{u^2} \left(\nu u_{yy} - \frac{P_x}{\rho} \right). \quad (2.13)$$

If turbulent advection is omitted from ODT, then the stochastic simulation reduces to a deterministic numerical solution of (2.7) or (2.12), as applicable, and hence to a solution of the corresponding laminar initial-boundary-value problem. The numerical method, discussed in Appendix A, is necessarily different from methods tailored to laminar problems, owing to strong velocity gradients that develop when the turbulent advection process is included.

2.3.2. Small-eddy suppression

Though viscous evolution as outlined in §2.3.1 suppresses small-scale u fluctuations, it does not prevent small mappings driven by large-scale fluctuations. In fact, for fixed velocity gradient $\Delta u/l$, τ is independent of l and λ is proportional to l^{-2} , diverging as $l \rightarrow 0$. Despite this divergence, the effect of small mappings is minor because their contribution to transport scales as l^2/τ , and thus as l^2 for fixed $\Delta u/l$.

This has been confirmed numerically by running representative cases at successively higher resolutions to verify that results become independent of resolution, and thus independent of the size of the smallest resolved mapping.

It is physically more appealing to recognize that the occurrence of these small mappings is an artifact of the distinction between mappings and the u profile, and therefore to suppress mappings that are incommensurate with the length scales of u fluctuations. This suppression of small mappings is formulated to reflect the viscous mechanism that suppresses the small-scale u fluctuations. Namely, a mapping is suppressed if its time scale τ is longer than a time scale $\tau_d = l^2/(16\nu)$ that governs viscous suppression of the eddy motion. The origin of the numerical factor is explained in Appendix A. Note that τ_d is a rapidly increasing function of l , so its effect is to suppress small eddies. (τ is typically a less rapidly increasing function of l .)

In §3.2.4, simulations with and without small-eddy suppression are compared, demonstrating that the effect of allowing the anomalous small eddies is minor for shear-driven flow. However, there is a class of buoyancy-driven flows for which small-eddy suppression is essential, as explained in §2.4.1.

2.4. Buoyancy

2.4.1. Generalized eddy rate distribution

Equation (2.3) can be recast in a form that allows generalization to buoyant flow. For this purpose, the total kinetic energy of the mapping-induced motion (the ‘eddy kinetic energy’) is evaluated.

For clarity, consider triplet-map implementation on a discretized domain, implemented as a permutation of the cells of the mapping interval (§2.2.1). The mapping-induced displacement δ of a given cell implies a cell velocity v based on the assumption that the time duration of the corresponding eddy in continuum flow is τ . Thus, the estimate $v = \delta/\tau$ is adopted. In Appendix C, it is shown that this relation can be used to extract v fluctuation statistics from simulated realizations.

The corresponding cell kinetic energy is $\frac{1}{2}\rho w v^2 = \frac{1}{2}\rho w \delta^2/\tau^2$, where w is the cell width and ρ is the cell density, expressed as mass per unit width. (The dimensions of density do not affect computed results because they are presented in non-dimensional form.) Here, the Boussinesq approximation is adopted, so ρ is set equal to a reference density ρ_0 except in terms involving the gravitational acceleration g . (The model can be extended to include some non-Boussinesq effects, but this is not implemented here.)

Summing over mapped cells, the total kinetic energy of the mapping-induced motion (the ‘eddy kinetic energy’) is $\frac{1}{2}\rho_0 l \langle \delta^2 \rangle / \tau^2$, where $\langle \delta^2 \rangle$ is the mean-square fluid displacement in the mapping interval. For the triplet map (spatial continuum definition), $\langle \delta^2 \rangle = \frac{4}{27} l^2$ (Kerstein 1991), so the eddy kinetic energy becomes $\frac{2}{27} \rho_0 l^3 / \tau^2$.

A kinetic energy density is obtained by dividing this quantity by l . Introducing the expression (2.3) for τ , the relation $\frac{2}{27} \rho_0 (l/\tau)^2 = \frac{2}{27} \rho_0 (A\Delta u)^2$ can be interpreted as a vortical kinetic energy density (left-hand side) fed by the kinetic energy of the local shear (right-hand side). The proposed generalization to buoyant flow is

$$\frac{2}{27} \rho_0 \left(\frac{l}{\tau} \right)^2 = \frac{2}{27} \rho_0 (A\Delta u)^2 - \frac{\Delta E_g}{l}, \quad (2.14)$$

where

$$\Delta E_g = g \int [\hat{\rho}(y) - \rho(y)] y \, dy \quad (2.15)$$

is the change in gravitational potential energy upon application of a triplet map to

the segment $[y_0, y_0 + l]$. In (2.15), ρ and $\hat{\rho}$ respectively are the density profiles before and after the application of the map.

Equation (2.14) is analogous to an expression formulated by Stull & Driedonks (1987) to determine the fluid-exchange time scale in their one-dimensional model of time-average vertical turbulent transport in buoyant flow. Aside from being an instantaneous rather than a time-average relation, the main difference between (2.14) and their expression is the omission of energy dissipation from (2.14). This and other aspects of buoyant-flow energetics in ODT are discussed in §2.4.2.

Stull & Driedonks (1987) motivate their formulation by a closure of the turbulent kinetic energy equation. Equation (2.14) can be regarded as an instantaneous analogue of their formulation. However, (2.14) can be rationalized without reference to closure modelling: it is obtained by assuming the additivity of kinetic and potential energy contributions to vorticity production, and by requiring that (2.14) reduces to (2.3) for constant-density flow.

In stable stratification, (2.14) can give a negative value on the right-hand side. Application of the triplet map to $[y_0, y_0 + l]$ is then deemed to be energetically forbidden, so the map is prevented from occurring by setting τ equal to infinity. A map on this interval may become energetically allowed at a later time, with a commensurate value of τ , depending on the subsequent evolution of the u and ρ profiles.

In applications considered here, density fluctuations are caused by temperature variations imposed on the flow. The molecular transport of heat can be represented by an equation of the form (2.8), with density determined from the equation of state. For Boussinesq flow at low Mach number, density fluctuations are roughly proportional, and opposite in sign, to temperature fluctuations. Therefore density can be regarded as a diffusive scalar governed by

$$\rho_t = \kappa \rho_{yy}, \tag{2.16}$$

where κ is the thermal diffusivity. This formulation, which is a standard approximation for low-Mach-number Boussinesq flow, is adopted here.

Within this framework, the Richardson number

$$Ri = \frac{\Delta\rho gL}{\rho_0 U^2} \tag{2.17}$$

and the Rayleigh number

$$Ra = \frac{\Delta\rho gL^3}{\rho_0 \kappa\nu} \tag{2.18}$$

are defined in the usual manner in terms of length and velocity scales L and U , and a density difference $\Delta\rho$, that are specified for each flow configuration. Scaling all dimensional quantities in (2.14) and (2.15) in terms of L , U , and ρ_0 ,

$$\left(\frac{l}{\tau}\right)^2 = (A\Delta u)^2 - \frac{27Ri}{2l} \int [\hat{\rho}(y) - \rho(y)]y dy \tag{2.19}$$

is obtained, where all quantities are now non-dimensional.

For flows that involve characteristic length and velocity scales L and U , the non-dimensional formulation is parameterized by Ri , by the Reynolds number $Re = UL/\nu$, and by the Prandtl and Schmidt numbers (Pr , Sc) governing the molecular diffusion of heat and any other diffusive scalars advected by the flow. If there is no characteristic

velocity scale, then the normalizing velocity U is replaced by v/L , giving

$$Ri = Ra/Pr, \quad (2.20)$$

where $Pr = \nu/\kappa$. Thus, the usual parameterization by Ra and Pr (plus any applicable Schmidt numbers) is obtained for flows of this type.

These flows are typically buoyant flows driven by locally unstable vertical variations of density. An unstably stratified density profile can generate a self-sustaining cascade of mapping events, irrespective of shear contributions. For unstably stratified flows with no applied shear or pressure gradient, the velocity profile $u(y, t)$ is identically zero initially and is not modified by mappings or by viscous evolution, so it is effectively decoupled from the simulated flow evolution. This special case of ODT is denoted density-profile evolution (DPE). All computed results presented in §5 are obtained using DPE. In DPE, small-eddy suppression is the only operative mechanism representing viscous effects, and thus is the mechanism that governs Pr dependences.

2.4.2. Buoyant-flow energetics

Equation (2.14) implies the conversion of gravitational potential energy into vertical kinetic energy. This picture is oversimplified in several respects.

First, it neglects the conversion of a portion of the gravitational potential energy into horizontal kinetic energy. This tends to cause an excessive intensity of induced vertical motions. In DPE, horizontal motions play no explicit role in flow evolution. In ODT with buoyancy and shear, only the shear forcing can contribute to the total horizontal kinetic energy. Vertical motions generated by buoyant forcing cannot affect the total horizontal kinetic energy because the y -integral of u^2 (or of any other function of u) is invariant under mappings. However, buoyant forcing (or suppression, in stable stratification) can indirectly influence the viscous dissipation of horizontal kinetic energy through the effect of mappings on the length scale of u -profile fluctuations.

Second, it is implicit in the model that the vertical kinetic energy associated with a mapping is entirely dissipated by that motion. There is no provision within the model for that energy to drive subsequent motions, horizontal or vertical. In principle, it is possible to define the vertical kinetic energy locally within ODT, with (2.14) generalized accordingly. This would allow a local, instantaneous energy balance, including a physically based mechanism for dissipating vertical kinetic energy. However, the assumption that an eddy dissipates its kinetic energy in one turnover is not a drastic oversimplification. The mechanism of this dissipation is energy transfer to smaller-scale, shorter-lived motions, i.e. the turbulent cascade, terminating at the viscous-dissipation length scales after a delay of the order of the eddy-turnover time.

For buoyancy-driven turbulence, details of the conversion of vertical kinetic energy to other forms are generally unimportant because the prior step of potential energy conversion to vertical kinetic energy dominates the flow kinematics. This point is elaborated in the discussion of the Bolgiano–Obukhov scaling of the ODT buoyancy-driven cascade (§5.1).

In contrast, important features of stably stratified turbulence are sensitive to the conversion of vertical kinetic energy to other forms (heat, horizontal kinetic energy, gravitational potential energy, and acoustic waves). The impact of the omission of these conversion processes on ODT simulations of stably stratified flow regions is noted in §5.3 and §6.3.

The cascade of horizontal kinetic energy is explicitly represented in shear-driven ODT through the coupling between the u profile and the event-rate distribution

(§2.2.2). With or without buoyancy, the ODT budget of the u component of turbulent kinetic energy, $\langle u^2 \rangle / 2$, is self-contained. For non-buoyant shear-driven flow, this budget is interpreted in Appendix B as the model analogue of the total (sum over velocity components) turbulent kinetic energy budget. This is fairly accurate for boundary-layer-type flows in which turbulence production is driven by the y variation of u . For isotropic turbulence, however, $\langle u^2 \rangle / 2$ is interpreted as one-third of the total turbulent kinetic energy. Thus, the ODT analogue of the energy-dissipation rate is

$$\epsilon_{\text{ODT}} = cv \langle (du'/dy)^2 \rangle, \quad (2.21)$$

where $c = 1$ for boundary-layer flows and $c = 3$ for isotropic turbulence.

Equation (2.21) is generalized to incorporate sources and sinks of gravitational potential energy as follows. In accordance with (2.14), it is assumed that a mapping-induced potential-energy decrement corresponds to a vertical-kinetic-energy increment that is immediately dissipated. A potential-energy increment is possible if there is shear forcing sufficient to make the right-hand side of (2.14) positive. This energy storage mechanism is represented by decrementing the energy dissipation, so that the aggregate energy dissipation balances the turbulent-kinetic-energy production (Appendix C) minus the net potential energy change.

These considerations motivate generalization of (2.21) by subtracting the buoyancy flux, giving

$$\epsilon_{\text{ODT}} = cv \langle (du'/dy)^2 \rangle - (g/\rho_0) \langle \rho' v' \rangle. \quad (2.22)$$

For DPE, in which the u profile is absent, the additional term is the sole contribution to ϵ_{ODT} . For this case, (2.22) reflects the assumed immediate dissipation of gravitational-energy losses.

In general, the justification for (2.22) is qualitative at best. For stably stratified flows that are initially isotropic, (2.22) correctly implies less dissipation than for isotropic turbulence with the same value of $\langle u^2 \rangle$. However, the complexities of energy transfers involving gravitational energy and the velocity components are not captured. This reflects the primarily kinematical nature of ODT, with dynamical considerations represented only in a limited sense, through (2.14) and (2.15). Therefore (2.22) should be regarded as a postulated interpretation of ODT whose degree of validity must be assessed empirically.

2.5. Parameter evaluation

ODT involves a single free parameter A in the relation (2.19) determining the eddy time scale. Multiplying the viscous equation (2.7) and the initial and boundary conditions for u by A , it is evident that for T-flows, A and u appear only in the combination Au (except in the P_x term, which is absent in cases considered here). Taking U and L to be characteristic velocity and length scales, a simulation for given A and U is therefore equivalent to a simulation for any $A' \neq A$ with rescaled characteristic velocity $U' = (A/A')U$. The respective Reynolds numbers are $Re = UL/\nu$ and $Re' = U'L/\nu$, indicating the Re rescaling $Re' = (A/A')Re$. Likewise, $Ri' = (A'/A)^2 Ri$.

The relation $dx = u dt$ between streamwise increments dx and Lagrangian time increments dt in S-flow implies the rescaling $dx' = (A/A')dx$. Equations (2.9)–(2.11) are invariant under the simultaneous application of this transformation and $u' = (A/A')u$, showing that the stated Re and Ri rescalings apply also to S-flow.

A can be determined empirically or by invoking a self-consistency condition. If the latter, then the model becomes wholly self-contained. DPE (§2.4.1) is likewise self-contained because in DPE, the term containing A drops out of (2.19).

The evaluation of the transverse velocity variance $\langle v'^2 \rangle$ in ODT is explained in Appendix C. Because both $\langle u'^2 \rangle$ and $\langle v'^2 \rangle$ can be obtained from simulated realizations, relaxation to isotropy in ODT simulations of homogeneous turbulence can be enforced by requiring $\langle v'^2 \rangle = \langle u'^2 \rangle$ in the regime of self-similar evolution. Based on computations discussed in §3.2.4, this procedure gives $A = 0.82$. This differs from the value $A = 0.3$ required to match the measured value of the Kolmogorov constant (§3.2.2).

Two shear flows are considered here: Couette flow and the planar boundary layer. The empirical considerations determining A for non-stratified and stratified Couette flow are discussed in §4 and §6.1. The planar boundary layer is considered in the context of entrainment of stably stratified fluid. It is shown in §6.3 that application of a mathematical stability criterion for the onset of shear-driven entrainment yields $A = 0.5$.

The difference between this and the value $A = 0.82$ obtained from isotropy considerations indicates that the present formulation does not simultaneously satisfy all known mathematical requirements for a fully quantitative analogy to three-dimensional flow. This could perhaps be remedied by introducing additional free parameters. Possibilities in this regard are noted in §2.2 and Appendix C. The present focus is the comparison of computed and measured trends and features for purposes of mechanistic interpretation. Therefore, efforts to achieve consistent quantitative accuracy are not pursued here.

3. Homogeneous turbulence

3.1. Eddy cascade

The ODT representation of the microstructure of turbulence, and of passive scalars advected by turbulence (parameterized by the Prandtl number $Pr = \nu/\kappa$), is considered. First, the mechanism that induces an eddy cascade within ODT is examined. Consider the initial-value problem $u(y, 0) = y$, representing a uniform imposed shear. According to (2.6), this yields the eddy rate distribution $\lambda \sim l^{-2}$, independent of y_0 . With the occurrence of mappings, $u(y, t)$ is changed. To determine the effect on λ , consider $u(y, t)$ after the occurrence of a single mapping of given size l . Within each subinterval of the mapping interval (see (2.1)), the shear is tripled, causing a tripling of λ for eddies contained within the subinterval. Thus, mapping events increase the subsequent rate of occurrence of smaller events contained within them. The iteration of this rate multiplication over successively smaller length scales is the mechanistic basis for the occurrence of an eddy cascade within ODT.

The steepening of gradients and the wrinkling of the profile $u(y, t)$ by mappings is counteracted by the smoothing effect of the concurrent viscous process. The dominant process at given l can be determined by comparing advective and viscous time scales. Based on (2.3), the advective time scale is of order l/δ_l , where δ_l is a characteristic velocity difference over a distance l . The viscous time scale is of order l^2/ν . Advection dominates provided that $l/\delta_l \ll l^2/\nu$, or equivalently, $l\delta_l/\nu \gg 1$, where $l\delta_l/\nu$ is a Reynolds number for length scale l . If this inequality is obeyed for some l , then there is a range of scales above l in which viscous inhibition of the cascade is negligible. This is the model analogue of the inertial range of turbulence. Further application of this reasoning suggests a transition to a viscous-dissipation range for small enough l .

The dimensional reasoning usually applied to turbulence scaling properties may carry over, to some extent, to ODT. The reason is that the dimensional relations determining turbulence scalings are implicit in two fundamental properties of the

model. Namely, (2.3) enforces the dimensionally correct dependence of the advection time scale on l and δ_l , while (2.7) or its S-flow analogue provides a literal implementation of viscous dissipation, albeit in one spatial dimension. A heuristic discussion of the ODT analogues of various scaling properties of homogeneous turbulence is presented, followed by examination of numerical results.

3.1.1. Inertial-range scaling

The first scaling to be considered is the inertial-range scaling of the energy spectrum of transverse velocity fluctuations, here denoted $E(k)$. Except for a low-wavenumber scaling considered in §3.2, the scaling properties of the transverse spectrum and of the three-dimensional spectrum are the same so the distinction between these is immaterial.

The Kolmogorov cascade picture that yields the scaling $E(k) \sim k^{-5/3}$ is summarized. It is assumed that the transport of kinetic energy in wavenumber space is local and non-dissipative from the energy-containing scales down to the viscous scales. This identifies the energy dissipation ϵ as the only relevant parameter (subject to intermittency corrections discussed shortly). The relation

$$E(k) = \frac{24}{55} C_K \epsilon^{2/3} k^{-5/3}, \quad (3.1)$$

where C_K is the ‘Kolmogorov constant,’ is then obtained as the unique dimensionally consistent scaling law for $E(k)$.

The factor $\frac{24}{55}$ arises because C_K is the amplitude coefficient of the three-dimensional energy spectrum, but $E(k)$ here denotes the energy spectrum of transverse velocity fluctuations (Appendix B). The inertial-range amplitude ratio $\frac{24}{55}$ for these spectra follows immediately from the relation between the spectra (Hinze 1975).

The underlying assumptions of local and non-dissipative energy transfer are obeyed by ODT, admitting the possibility of a Kolmogorov-type cascade in ODT. In the inertial range of ODT, the viscous process is irrelevant and the mappings determine the scaling properties. Because each mapping is a measure-preserving rearrangement of the u profile, the mappings preserve the integral of u^2 over the one-dimensional domain. In fact, they preserve the integral of any moment of u over the domain. (This property of ODT is reminiscent of incompressible two-dimensional Navier–Stokes turbulence, in which any moment of the vorticity field is conserved by advection. In other respects, the ODT cascade more closely resembles three-dimensional than two-dimensional turbulence.)

Moreover, the transfer of spectral intensity of any function of u is predominantly local in wavenumber. The threefold compression induced by each map corresponds to a threefold increase of the characteristic wavenumber of profile fluctuations within the segment. (There is also some spectral transfer to much higher wavenumbers because the map introduces discontinuous derivatives.)

Because the ODT inertial-range cascade conserves u^2 and is predominantly local in wavenumber, the reasoning originally used to derive (3.1) is applicable. Namely, the mean flux of kinetic energy to higher wavenumbers is the same at all wavenumbers, and therefore is equal to ϵ , here interpreted as the mean rate of energy input at low wavenumbers. (This interpretation is based on the usual equilibrium picture in which the low-wavenumber energy input balances the high-wavenumber energy dissipation. ODT can also simulate non-equilibrium transient flows in which the inertial-range spectrum may deviate from Kolmogorov scaling.) The assumption that $E(k)$ can therefore depend only on ϵ and k then implies (3.1).

The usual caveat is likewise applicable. In ODT, as in three-dimensional flow, the

local instantaneous value of ϵ is a random variable. The assumption that only its mean value enters the scaling is simple and well validated empirically, but deviations from (3.1) due to fluctuation effects (i.e. intermittency corrections) are not *a priori* excluded. This point is discussed further in §3.2.2.

3.1.2. Viscous-range scaling

As explained in §2.3, viscous effects are implemented in ODT by continuous-time evolution of $u(y, t)$ and by a small-eddy-suppression mechanism. Viscous-range scaling is considered initially with respect to the continuous-time evolution process only. In §3.2.4, the effect of small-eddy suppression on viscous-range scaling is discussed and demonstrated numerically.

The inertial-range scaling is applicable at length scales l for which $l\delta_l/\nu \gg 1$. For l small enough so that this inequality is reversed, viscous effects become dominant. The transition between regimes occurs for l of order ν/δ_l . The analysis of the ODT inertial range indicates that δ_l obeys the scaling that follows from the Kolmogorov cascade picture. The transition length scale for ODT is therefore the usual Kolmogorov microscale, $\eta = (\nu^3/\epsilon)^{1/4}$.

At length scales $l \ll \eta$, viscosity smooths eddy-induced fluctuations on a time scale $t_l \sim l^2/\nu$ that is much shorter than the eddy time scale τ_l . Therefore $u(y)$ in the viscous-dominated range is effectively a constant-gradient profile punctuated by mapping-induced fluctuations that vanish rapidly, and hence have negligible effect on the rate of subsequent mapping events. τ_l in the viscous range can therefore be estimated by taking the velocity difference in the denominator of (2.3) to be proportional to l , giving τ_l independent of l .

This allows a simple estimate of the kinetic-energy spectrum in the viscous range. Dimensionally, $E(1/l) \sim \delta_l^2 l$, where the parameterization $k = 1/l$ is used for convenience. Size- l mappings applied to a constant-gradient u profile induce order- l fluctuations, giving $\delta_l^2 \sim l^2$. Owing to the rapid smoothing of these fluctuations relative to their rate of creation, only a fraction $t_l/\tau_l \ll 1$ of the spatial domain exhibits significant fluctuations at any instant. Multiplying δ_l^2 by this fraction and substituting the l dependencies of the time scales, the spectral scaling $E(k) \sim k^{-5}$ is obtained in the viscous range.

This is a slower falloff than indicated by analysis and three-dimensional numerical simulation of the viscous range (Sirovich, Smith & Yakhot 1994). Small-eddy suppression steepens the falloff somewhat (§3.2.4), but slower-than-observed falloff persists owing to the high-wavenumber content of the discontinuous derivatives introduced by the triplet map.

3.1.3. Advected scalars: Pr dependence

Provided that $P_x = 0$ in (2.7), the velocity profile $u(y, t)$ in ODT evolves in the same manner as a passive scalar that is subject to the same initial and boundary conditions, and that has molecular diffusivity κ equal to ν , i.e. $Pr = 1$. Thus, the earlier discussion of scaling properties of u carries over to a passive scalar with $Pr = 1$.

In particular, this equivalence implies $E_\theta = E$, where E_θ is the one-dimensional scalar spectrum with the normalization stated in Appendix B. In the inertial-convective range, E_θ obeys the scaling (Lesieur 1990)

$$E_\theta(k) = C_\theta \epsilon \nu^{-1/3} k^{-5/3}. \quad (3.2)$$

Equations (3.1) and (3.2) give

$$\frac{E_\theta}{E} = \frac{55}{24} \frac{C_\theta}{C_K} \frac{\epsilon_\theta}{\epsilon} \quad (3.3)$$

for k such that both scalings are obeyed. Based on $E_\theta = E$ and the measured values $C_K = 1.5$ (Sreenivasan 1995) and $C_\theta = 0.8$ (Sreenivasan 1996), equation (3.3) gives $\epsilon/\epsilon_\theta = 1.2$. (C_K and C_θ here denote Sreenivasan's quantities $\frac{55}{18}C_K$ and $2C_\theta$ respectively.) This tends to favour the definition of ϵ based on the dynamical analogy (giving $\epsilon/\epsilon_\theta = 1$) over the kinematical analogy (giving $\epsilon/\epsilon_\theta = 3$) that is adopted in Appendix B. Further consideration of the criterion for defining ϵ in ODT is warranted.

For $Pr \ll 1$, analysis and computations based on the LEM (Kerstein 1991) indicate that the scaling properties of the LEM inertial-diffusive range are slightly different from those presumed to govern turbulent flow. The discrepancy, explained in detail in the cited reference, is anticipated to occur in ODT as well. Scalars with $Pr \ll 1$ are not investigated here.

For $Pr \gg 1$, molecular-diffusive effects are significant at length scales l for which the diffusion time scale $t_l \sim l^2/\kappa$ is less than the eddy time scale τ_l . As shown in § 3.1.2, τ_l is independent of l in ODT for $l \ll \eta$, and thus is of order $\tau_\eta \sim \eta^2/\nu$. The Batchelor scale L_B marking the transition to molecular-diffusion dominance is determined by equating the diffusion and eddy time scales, giving $L_B \sim Pr^{-1/2}\eta$. This is the same as the result obtained from the conventional analysis (Lesieur 1990) that assumes the suppression of eddies smaller than η . The ODT result is unaffected by the presence of eddies smaller than η because they do not introduce advective time scales shorter than τ_η . This indicates that the excessive frequency of small eddies in ODT may not have much impact on viscous-range properties of interest.

A corollary of this reasoning is that ODT spectra of high- Pr scalars should obey $E_\theta \sim \epsilon_\theta \epsilon^{-1/3} k^{-5/3}$ in the inertial range $l \gg \eta$, $E_\theta \sim \epsilon_\theta (\nu/\epsilon)^{1/2} k^{-1}$ in the viscous-convective range $\eta \gg l \gg L_B$, and $E_\theta \sim L_B \epsilon_\theta (\nu/\epsilon)^{1/2} (L_B k)^{-5}$ in the viscous-diffusive range $L_B \gg l$. Again, the ODT analysis parallels the conventional analysis (Lesieur 1990), except that considerations analogous to those of § 3.1.2 govern the viscous-diffusive range.

3.2. Numerical results

3.2.1. Simulated flow configurations

ODT simulations of three T-flow configurations demonstrate the scalings discussed in § 3.1. Two configurations involve sinusoidal initial u profiles, $u(y, 0) \sim \sin(2\pi y/L_0)$, with periods $L_0 \ll Y$ and $L_0 = Y$ respectively, where Y is the size of the computational domain. For these configurations, periodic boundary conditions are applied. For the first configuration, the simulation is restricted to a time interval over which the flow macroscale L defined by (B 6) remains much smaller than Y , so the domain is effectively infinite. This configuration corresponds to freely decaying turbulence. The second configuration represents bounded decaying turbulence.

The third configuration corresponds to statistically stationary turbulence, forced by the imposition of a constant (in y) initial shear $u(y, 0) = y/Y$ and jump-periodic boundary conditions, $u(y + jY, t) = u(y, t) + j$ for any integer j . To prevent the dominance of eddies larger than Y , mappings of size $l > Y$ are disallowed.

The second and third configurations do not correspond to physically realizable flows, but they are useful for demonstrating phenomena that occur in real flows. Direct numerical simulation (DNS) and large-eddy simulation (LES) of these configurations have provided valuable insights, and provide a basis for interpretation of ODT results.

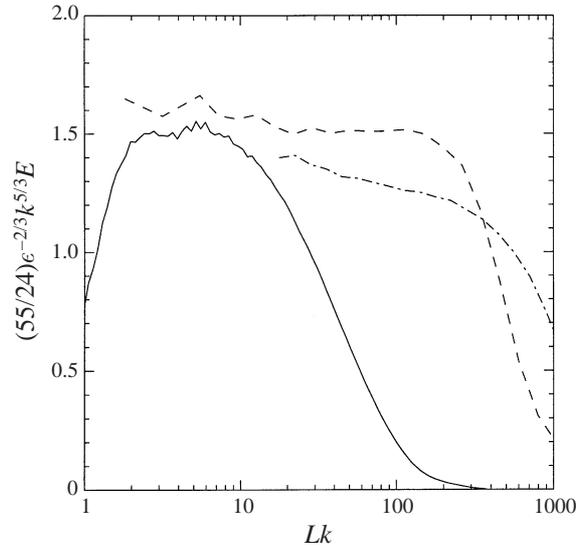


FIGURE 2. Power spectra of u , plotted in coordinates that demonstrate inertial-range scaling, for the cases shown in table 1: —, freely decaying turbulence; - - -, bounded decaying turbulence; - · -, stationary turbulence.

To illustrate the performance of the simplest possible formulation of ODT, the three configurations are simulated without invoking small-eddy suppression. To assess the impact of this, the first configuration is also simulated with small-eddy suppression included.

For the decaying cases, the sinusoidal initial profile is chosen for simplicity. After a transient interval, self-preserving decay is obtained that is insensitive to the functional form of the initial profile.

The similarity scalings governing the decay are not considered in detail. The ODT scalings are found to be consistent with the scaling laws known to govern freely decaying turbulence (Chasnov 1994) and bounded decaying turbulence (Borue & Orszag 1995), except that ODT low-wavenumber spectra in the former case scale as k^2 rather than k^4 . This difference is a direct consequence of the one-dimensional formulation (Kerstein & McMurtry 1994*b*). Turbulence decay in ODT is therefore governed by slightly different scaling laws than those presumed to govern three-dimensional flow; see Chasnov (1994) for a discussion of the relationship between low-wavenumber spectra and decay rates.

3.2.2. Spectral scalings: velocity

To test for inertial-range scaling, (3.1) is expressed in the form $C_K = \frac{55}{24}\epsilon^{-2/3}k^{5/3}E(k)$. In figure 2, the right-hand side of this relation is plotted versus k in order to demonstrate the occurrence of the $k^{-5/3}$ scaling, indicated by a plateau in the plot. For all three flows, the model parameter A is assigned the value 0.3, chosen to match the plateau level for the bounded decaying case to the measured value $C_K = 1.5$ (Sreenivasan 1995). A determines the plateau level through the expression (B 1), or equivalently (B 2), for ϵ , where time and viscosity in those expressions depend on A as explained in §2.5.

A Reynolds number $Re_L = \langle u^2 \rangle^{1/2}L/\nu$ is formed using the definition (B 6) of L . For simulations of each of the three homogeneous-flow configurations, values

| | Free decay | Bounded decay | Stationary |
|------------|------------|---------------|------------|
| Re_{L_0} | 4600 | 118 000 | 167 000 |
| Re_L | 330 | 6720 | 2000 |
| ζ | 1.67 | 1.67 | 1.73 |

TABLE 1. Computed inertial-range spectrum scaling exponents for three homogeneous flows.

of Re_L corresponding to plotted spectra are shown in table 1. Also shown are nominal initial Reynolds numbers Re_{L_0} of the simulated flows. For the decaying flows, $Re_{L_0} = \langle u'^2 \rangle_0^{1/2} L_0 / \nu$. For the stationary flow, $Re_{L_0} = \langle du/dy \rangle Y^2 / \nu$.

After an initial transient, each of the simulated flows relaxes to the anticipated asymptotic behaviour: stationarity for the stationary case and self-similar decay for the other cases. For the stationary case, spectral and other statistical quantities are accumulated continuously after transient relaxation is completed. For the free and bounded decaying cases, self-similar decay begins at $Re_L = 500$ and 7000 respectively. Table 1 indicates the values of Re_L corresponding to the results shown in figure 2, which are based on order 10^3 simulated realizations.

Figure 2 indicates a larger dynamic range of $k^{-5/3}$ scaling for bounded decay than for free decay, owing to the large Re_L value for the former. For the same A value, these two cases give the same C_K .

Numerical results for the exponent ζ in the scaling $E(k) \sim k^{-\zeta}$ are presented in table 1. The Kolmogorov scaling $\zeta = \frac{5}{3}$ is obeyed for the decaying flows but the stationary flow obeys power-law scaling with a different value of ζ .

It has been noted that departures from Kolmogorov scaling may be obtained in simulations of forced stationary turbulence, possibly associated with intermittency induced by the forcing (Borue & Orszag 1995). The ODT simulation of stationary turbulence involves an arbitrary eddy-size cutoff $l < Y$ that has no direct physical analogue. These observations do not fully resolve the status of the inertial-range scaling behaviour of ODT, but it can be stated that Kolmogorov scaling is obtained for the physically realizable cases that have been simulated.

The inference in § 3.1.2 that the Kolmogorov microscale η marks the transition from inertial to viscous dominance is tested by plotting spectra in universal dissipation-range coordinates. Figure 3 shows that dissipation-range collapse of spectra is obtained for all three homogeneous flows, including the stationary flow that deviates from $\zeta = \frac{5}{3}$ in the inertial range. Comparison to figure 2 indicates the high sensitivity of the figure 2 format to small deviations from $k^{-5/3}$ scaling.

A curve representing the dissipation-range rolloff of measured spectra is also shown. This curve was obtained by fitting She's analytical form (Sirovich *et al.* 1994) to a compilation of measured one-dimensional spectra (Monin & Yaglom 1975) and then applying the transformation (B 5) analytically to obtain the transverse spectrum directly comparable to ODT spectra.

As noted in Appendix B, a given energy dissipation rate corresponds to a larger mean-square velocity cross-derivative in ODT, based on (B 2), than in three-dimensional flow. Because the dominant contribution to ϵ is from the high-wavenumber end of the inertial range, this implies an extension of the ODT inertial range to larger ηk than in three-dimensional flow, as seen in figure 3. The k^{-5} scaling derived in § 3.1.2 for the far-dissipation range of ODT is not seen in this figure, but it is seen in lower- Re_L simulations that resolve more of the viscous range.

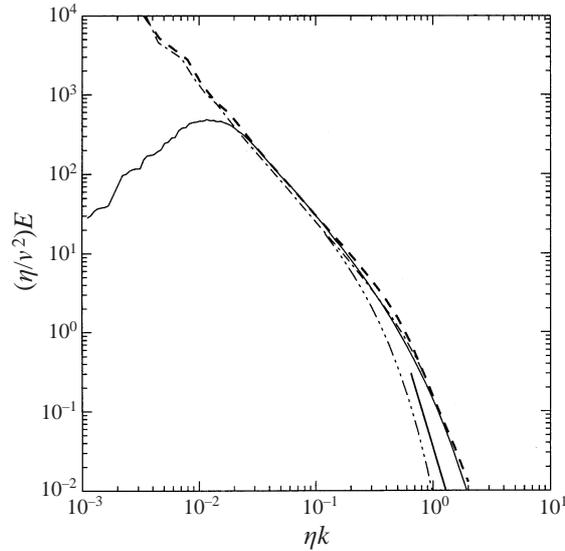


FIGURE 3. Power spectra of figure 2, replotted in universal dissipation-range coordinates; $-\cdots-$, measured spectrum. Line segment indicates k^{-5} scaling.

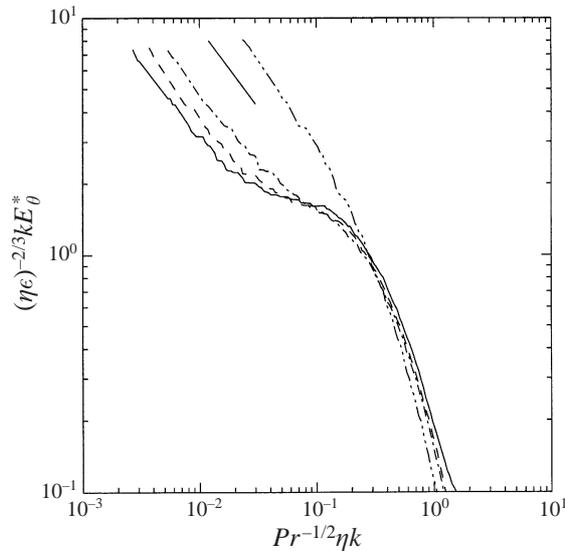


FIGURE 4. Power spectra of scalars in bounded decaying turbulence at $Re_L = 2040$, rescaled as explained in the text, plotted in universal high-wavenumber coordinates based on classical high- Pr theory, for $Pr = 1$ ($-\cdots-$), 20 ($-\cdot-$), 40 ($- - - -$), and 80 ($—$). Line segment indicates $k^{-5/3}$ scaling.

3.2.3. Spectral scalings: advected scalars

As explained in §3.1.3, the u profile can be interpreted as a passive-scalar field with $Pr = 1$. The viscous-convective scaling in ODT is investigated by comparing this scalar to other passive-scalar fields with $Pr \gg 1$, subject to the same initial and boundary conditions as u .

Results for the bounded decaying case are plotted in figure 4 in coordinates that

collapse the viscous-diffusive range $kL_B \gg 1$ according to the high- Pr scaling analysis of §3.1.3. The coordinates are defined so that $1/k$ spectral scaling corresponds to a plateau in the figure. The vertical axis is $(\eta\epsilon)^{-2/3}kE_\theta^*$, where $E_\theta^* = (\epsilon_1/\epsilon_\theta)E_\theta$. ($\epsilon_1 = \epsilon/3$ is the dissipation of the $Pr = 1$ scalar.)

Owing to the large dynamic range required to span the spectral ranges of interest, results are shown for $Re_L = 2040$, lower than the Re_L value of table 1 for this flow. Re_{L_0} for this computation is the same as in table 1, but the results of figure 4 correspond to a later stage of decay than the bounded-decay results of figure 2. Lower Re_L gives larger η and therefore more dynamic range allocated to the viscous regime.

For the Pr range shown in the figure, neither the viscous-convective spectral scaling nor the high-wavenumber collapse is fully attained. For the highest Pr shown, $E_\theta \sim k^{-1.1}$ at the inflection point of the plotted curve. In the dissipation range, the two intermediate- Pr curves suggest an approach to collapse, but the highest Pr does not maintain this trend. The slight flare at high wavenumbers for the highest Pr suggests aliasing caused by inadequate spatial resolution, so the apparent deviation from dissipation-range collapse may be a numerical effect. Nevertheless, it is evident that the computed results are broadly consistent with the classical high- Pr spectral scaling properties.

3.2.4. Freely decaying turbulence

Aspects of freely decaying turbulence are considered in §3.2.1 and §3.2.2. This flow is revisited for three reasons. First, small-eddy suppression is introduced in order to assess its impact on computed results. (All subsequent computations include small-eddy suppression.) Second, the isotropy condition (§2.5) is used to determine A , thereby eliminating the need for empirical input to determine A . Third, a procedure for determining the initial u profile corresponding to a turbulence-generating grid is formulated. This procedure introduces no empiricism. The predicted decay of grid turbulence, obtained computationally in this manner, is compared to experimental results.

In figure 5, the spectrum of figure 3 is replotted, along with two spectra from an identical computation, except that small-eddy suppression has been introduced. As in figure 3, the plotted results are based on $A = 0.3$, for which the measured value of the Kolmogorov constant C_K is reproduced. A slight but discernible effect on the shape of the spectrum is seen at the high-wavenumber end of the inertial range. The two curves based on the new formulation collapse in accordance with dissipation-range scaling.

The computation that includes small-eddy suppression is reinterpreted in the context of grid turbulence. The decay of velocity fluctuations in grid turbulence is considered. For this purpose, the isotropy condition $\langle u'^2 \rangle = \langle v'^2 \rangle$ is more relevant than the numerical value of C_K . Enforcement of this condition in the self-similar decay regime of the simulation gives $A = 0.82$. As noted in §2.5, the present formulation of ODT is not designed to reproduce all turbulence properties of interest with quantitative accuracy for a given A value.

It is also noted in §2.5 that a change of A value implies a rescaling of the Reynolds number associated with a given simulation. For $A = 0.82$, the simulation Reynolds number is $Re_{L_0} = 1680$ rather than the value indicated in table 1.

The initial velocity profile is $u(y, 0) = u_0 \sin(2\pi y/L_0)$, with L_0 set equal to the mesh spacing M of the turbulence-generating grid, and u_0 is chosen so that the u variance $u_0^2/2$ of $u(y, 0)$ is equal to a simple estimate of the variance of u in the plane of

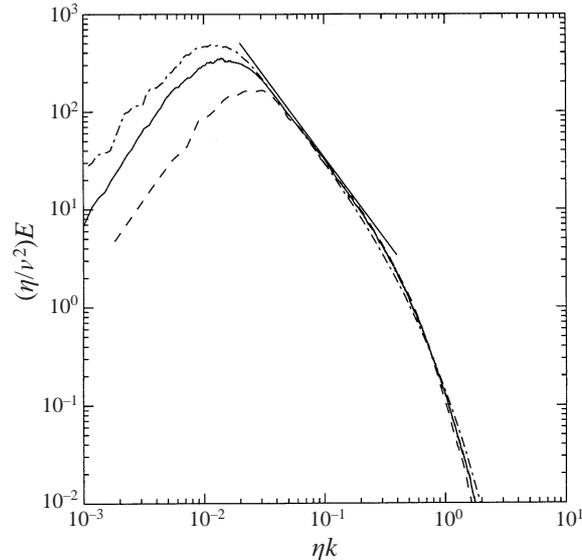


FIGURE 5. Computed power spectra of u in decaying homogeneous turbulence, plotted in universal dissipation-range coordinates. ($\eta = (\nu^3/\epsilon)^{1/4}$ is the Kolmogorov microscale.) $Re_L = 140$ (-----), 260 (—), and 330 (-·-), where $Re_L = \langle u^2 \rangle^{1/2} L/\nu$, based on $L = \langle u^2 \rangle^{3/2}/\epsilon$. The $Re_L = 330$ curve, replotted from figure 3, is from a simulation that omits small-eddy suppression. The other curves are from a simulation that incorporates small-eddy suppression. A line segment of slope $-\frac{5}{3}$ identifies the inertial range.

the grid. An estimate rather than a measured value is used in order to avoid the introduction of empiricism. Denoting the grid solidity as S , it is assumed that the flow in the grid plane consists of an area fraction S for which $u = 0$ and a fraction $1 - S$ for which u has the constant value $U/(1 - S)$, chosen so that the mean flow in the grid plane matches the mean flow U in the homogeneous region downstream of the grid. This gives a grid-plane u variance $U^2 S/(1 - S)$ and thus $u_0 = U\sqrt{2S/(1 - S)}$. For the experiments considered here, $S = 0.34$. Computational time is converted to streamwise distance using the relation $x = Ut$.

Figure 6 compares the computed decay of u and v variance to empirical far-field correlations (Yoon & Warhaft 1990) for decaying grid turbulence. It is seen that reasonable quantitative agreement is obtained over the streamwise range of typical grid-turbulence experiments (ranging up to x/M of several hundred), despite the complicated near-field behaviour of this flow. The persistent small-scale anisotropy of this flow, reflected in the empirical correlations, is not reproduced because isotropy has been deliberately enforced.

This ODT grid-turbulence model may be useful for addressing aspects of grid turbulence, and passive-scalar mixing therein, that have been examined experimentally. In this regard, the artifact discussed in Appendix A is relevant. Namely, large eddies with τ values greatly exceeding the elapsed time t occur infrequently in ODT, but their effect on transport is disproportionate. In particular, the root-mean-square (r.m.s.) fluctuation of a scalar with non-zero mean gradient is determined by the scalar displacements in the gradient direction, and hence is sensitive to this anomalous transport. Consequently, it is found in ODT grid-turbulence simulations with an imposed scalar gradient that the streamwise profile of the scalar r.m.s. fluctuation exceeds the measured profile by roughly a factor of six, based on the empirical

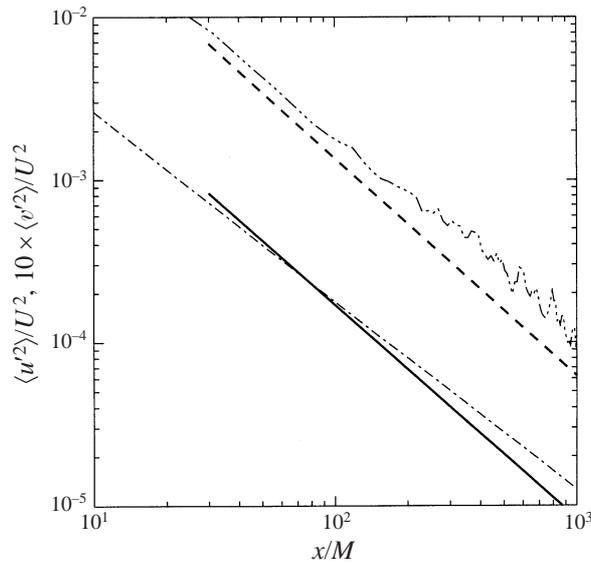


FIGURE 6. Computed evolution of streamwise and transverse velocity variance in decaying grid turbulence: —, streamwise variance; - - - -, transverse variance. Empirical correlations (Yoon & Warhaft 1990): — · —, $\langle u^2 \rangle / U^2 = 0.0712(x/M)^{-1.31}$; · · · · ·, $\langle v^2 \rangle / U^2 = 0.0652(x/M)^{-1.34}$.

correlation in figure 10 of Yoon & Warhaft (1990). Anomalous dispersion of scalars released from localized sources is likewise anticipated. This issue has been addressed in detail in the context of the LEM (Kerstein 1991, 1992; de Bruyn Kops & Riley 1998).

4. Wall-bounded flow

ODT simulations of Couette flow, channel flow, pipe flow (based on a cylindrical formulation not presented here), and the spatially developing planar boundary layer have been performed. Results are presented here for Couette flow, because it is the base case for stratified boundary-layer problems considered in § 6.

Couette flow is simulated by applying the boundary conditions $u(0, t) = 0$, $u(Y, t) = U$ to the computational domain $[0, Y]$. The initial velocity profile is linear, but this is immaterial because only the statistically steady flow that follows transient relaxation is considered. Following convention, this flow is characterized by the half-width Reynolds number $Re = UY/(2\nu)$.

The model parameter A is assigned the value 0.23 because this value is found to give a good match to the friction law and growth law of the spatially developing planar boundary layer. (Results for this flow are not presented here.) With this choice, Couette-flow results are compared to measurements without introducing additional empiricism.

Computed results are shown for $Re = 2900$ and $18\,000$, values for which Reichardt measured mean velocity profiles in Couette flow. Computed results are compared to his measurements, reported by Schlichting (1979), in figure 7. Reasonable overall agreement is obtained.

The computed mean velocity profiles are replotted in wall coordinates in figure 8. (Here, $u^+ = \langle u \rangle / u_\tau$ and $y^+ = yu_\tau/\nu$, where $u_\tau = (\nu d\langle u \rangle / dy|_{y=0})^{1/2}$ is the friction velocity.) Precise collapse of the wall-scaled profiles is obtained, with a wide zone

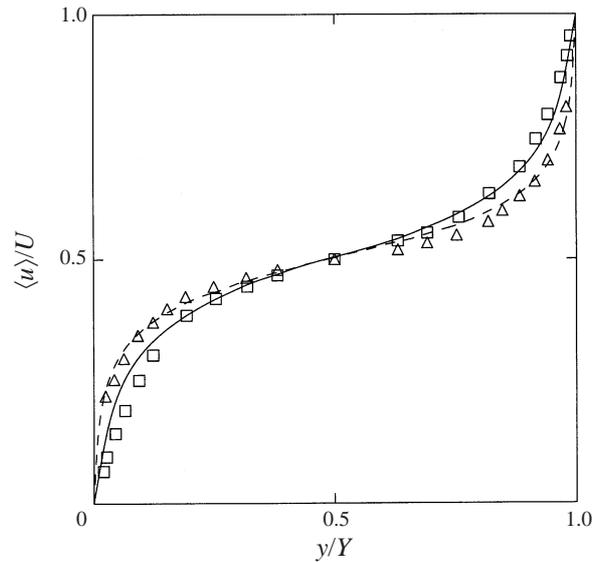


FIGURE 7. Mean velocity profiles in Couette flow. Computations: $Re = 2900$ (—), 18000 (----). Measurements by Reichardt (Schlichting 1979): $Re = 2900$ (\square), 18000 (\triangle).

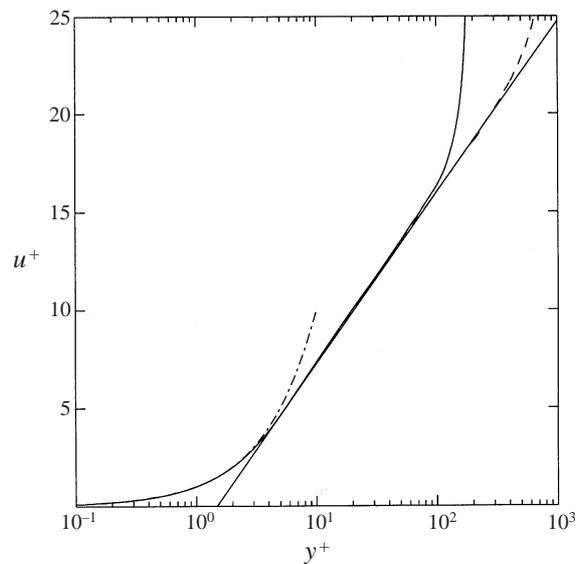


FIGURE 8. Computed mean velocity profiles of figure 7, replotted in wall coordinates. Also plotted are the functions $u^+ = 3.8 \ln y^+ - 1.5$ (—) and $u^+ = y^+$ (---) that identify the log-law and viscous layers, respectively.

of logarithmic dependence. The log-region scaling corresponds to a value $\kappa_V = 0.26$ of the von Kármán constant, close to the value 0.25 obtained from the spatially developing boundary-layer simulation. The measured value is 0.41 (Hinze 1975).

The conformance of the computed results to familiar scaling properties of the boundary layer stems largely from the fact that these properties can be derived from momentum conservation in conjunction with fairly mild assumptions concerning

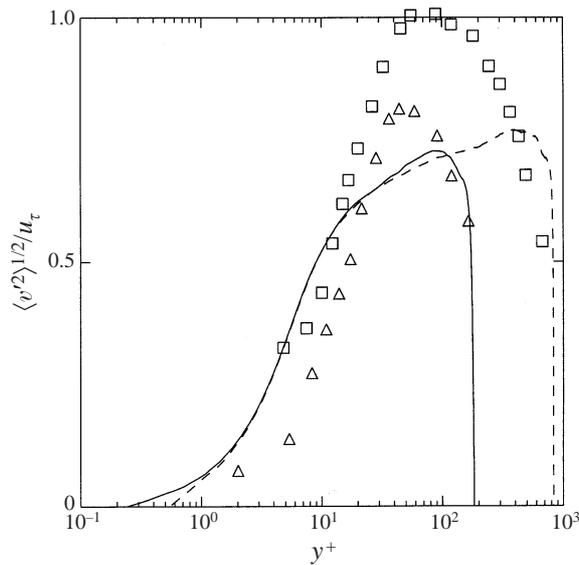


FIGURE 9. Transverse-velocity fluctuation profiles computed for Couette flow: $Re = 2900$ (—), 18000 (----). Measurements in channel flow (Wei & Willmarth 1989): $Re = 2970$ (Δ), 14914 (\square).

the structure of the near-wall and outer flows. These assumptions should be no less applicable to ODT than to three-dimensional turbulence. Nevertheless, it is noteworthy that ODT reproduces diverse facets of boundary-layer phenomenology within a simple modelling framework.

The computed profiles of $\langle v'^2 \rangle^{1/2}$, plotted in wall coordinates, are compared to channel-flow measurements (Wei & Willmarth 1989) in figure 9. The model underpredicts the peaks of the measured profiles roughly to the same extent that it underpredicts peaks of $\langle u'^2 \rangle^{1/2} / u_\tau$ profiles (not shown). Thus, the model is internally consistent in its representation of u and v fluctuations, lending support to the formulation of v fluctuation statistics in Appendix C. The degree of predictive accuracy indicated by figure 9 is typical of second-order fluctuation statistics computed for wall-bounded flows.

In figure 10, computed terms of the budget of $\langle u'^2 \rangle / 2$ for $Re = 2900$ are compared to the turbulent kinetic energy budget from channel-flow DNS at $Re = 3300$ (Mansour, Kim & Moin 1988). ($\langle u'^2 \rangle / 2$ is the model analogue of turbulent kinetic energy in boundary-layer flows, as explained in Appendix C.)

Comparisons by Mansour *et al.* (1988) and by Eggels *et al.* (1994) of the channel-flow results to results for the planar boundary layer and for pipe flow indicate that the near-wall energy balance is insensitive to flow configuration. Channel DNS at $Re = 7900$ (Antonia *et al.* 1992) indicates slight increases of the production peak and of the near-wall dissipation relative to the $Re = 3300$ results.

The DNS results are plotted on the negative y^+ -axis for ease of comparison. The computed terms of the balance, based on (C 6), are expressed in wall coordinates by normalizing by u_τ^4 / ν . In this plot, the scaling of the horizontal coordinate depends on A , but the height of the profiles does not.

The ODT energy balance is seen to be in fairly good quantitative as well as qualitative agreement with the DNS energy balance. This is possible only because pressure transport is a minor contribution to the energy balance in the boundary

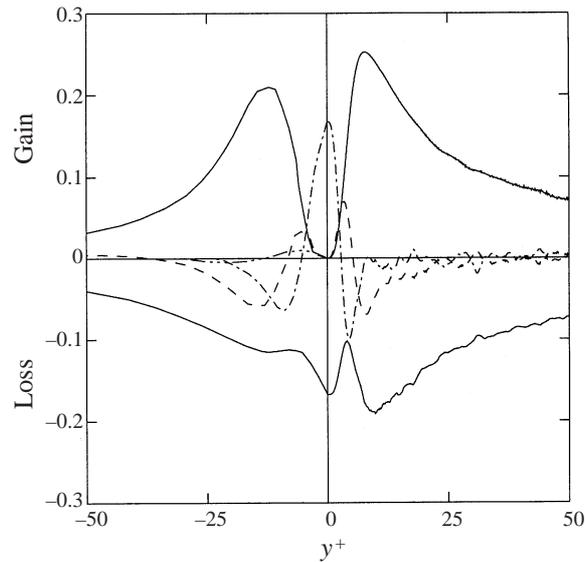


FIGURE 10. Computed near-wall turbulent kinetic energy balance in Couette flow based on ODT for $Re = 2900$ (positive y^+), and in channel flow based on DNS for $Re = 3300$ (Mansour *et al.* 1988; negative y^+): —, production (upper curve), dissipation (lower curve); ----, turbulent transport; - · - ·, viscous transport; · · · ·, pressure transport (DNS only; ODT has no pressure-transport mechanism).

layer, so its omission from ODT does not impose large perturbations on the other terms.

Numerous second-order closures, reviewed by So *et al.* (1991), have been proposed for near-wall turbulence. Several of them provide better overall representations of one-point statistics up to third order than does ODT. This comparison is noted in order to emphasize that the simple approach adopted here is neither designed nor intended to outperform models tailored to reproduce the low-order one-point statistics of particular flows. The present goal is to capture diverse features of many flows within a unified framework that allows straightforward extension to variable-property flows, reacting flows, and related problems. This addresses both the scientific goal of conceptual unification and the practical objective of reliably extrapolating from constant-property conditions to engineering problems involving many strongly coupled physical processes.

5. Buoyancy-driven flow

5.1. Homogeneous buoyancy-driven turbulence

As noted in §2.4.1, (2.14) implies a simple method for simulating buoyancy-driven turbulence with no applied shear. The u profile is omitted entirely, yielding self-driven density-profile evolution (DPE). All flows considered in §5 are simulated in this manner.

In buoyancy-driven turbulence, as in shear-driven turbulence, the most fundamental property is the eddy cascade. The buoyancy-driven cascade is not as well understood as the shear-driven cascade. Detailed assessments of recent theoretical and experimental work are provided by Grossmann & L'vov (1993) and by Siggia (1994).

Procaccia & Zeitak (1989) proposed that the temperature spectrum measured by Wu

et al. (1990) in buoyancy-driven turbulence could be interpreted as a manifestation of the Bolgiano–Obukhov (BO) scaling, originally predicted to occur in stably stratified turbulence. L’vov (1991) noted that the locality of interactions between eddies and density fluctuations implies that scaling in the buoyancy-dominated wavenumber range should be indifferent to the direction of the stratification. Various analytical and computational models of buoyancy-driven turbulence have subsequently reproduced the BO scaling.

Here, a scaling analysis is developed that reflects the presumed governing mechanism. The analysis is based on the features of buoyancy-driven turbulence that are incorporated into ODT, thereby identifying the origin of BO scaling within the ODT framework.

Density fluctuations are assumed to cascade toward high wavenumbers due to mapping-induced reduction of fluctuation length scales. Because mappings conserve all scalar properties, this cascade conserves the spectral intensity of density fluctuations, denoted ρ_k^2 , at wavenumbers k below the wavenumber range (identified shortly) in which molecular diffusion is significant.

Assume, subject to self-consistent verification, that the cascade time scale τ_k decreases with increasing k , so that the high- k cascade equilibrates rapidly with respect to low- k transients. A quasi-steady analysis can then be applied.

In a quasi-steady cascade that conserves ρ_k^2 , the flux of ρ_k^2 to higher k is of order ρ_k^2/τ_k and is independent of k , giving $\rho_k^2 \sim \tau_k$. (In this and subsequent scaling analyses, numerical coefficients are omitted.) The power spectrum $E_\rho(k)$ of density fluctuations, which scales dimensionally as ρ_k^2/k , is determined by $\rho_k^2 \sim \tau_k$ and one additional relation involving ρ_k and τ_k . The additional relation follows from (2.14) and (2.15), specialized to DPE. For $l = 1/k$, the density difference in the integrand of (2.15) is of order ρ_k and the y dy -integration introduces an additional factor of k^{-2} . Equation (2.14) then gives $\rho_0/(k\tau_k)^2 \sim \rho_k/k$. In conjunction with $\rho_k^2 \sim \tau_k$, this gives $\rho_k \sim k^{-1/5}$ and thus $E_\rho(k) \sim k^{-7/5}$, which is the BO scaling of the density spectrum.

This result may be interpreted as follows. Equation (2.14) implies that size- l eddies are driven by density fluctuations of comparable size. This locality property of the buoyancy-driven cascade, analogous to the presumed locality of the inertial cascade, has been proposed as the mechanistic basis of the dimensional relations underlying the BO scaling (L’vov 1991).

Because kinetic energy is not explicit within DPE, DPE cannot address the possibility that the kinetic-energy cascade, rather than the density cascade, governs buoyancy-driven turbulence. Evidence supporting this possibility is discussed by Siggia (1994).

To derive crossovers from BO scaling to other scaling regimes, consider the following initial-value problem for ODT. A constant, unstable density gradient is imposed initially on a size- Y domain. Jump-periodic boundary conditions, as defined in § 3.2.1, are applied in order to emulate an imposed density gradient on an unbounded domain. Mappings larger than Y are disallowed. This restriction is arbitrary from a physical viewpoint, but convenient for deriving and computationally demonstrating scalings of interest.

A large- k crossover to a regime dominated by molecular transport occurs at a wavenumber such that the eddy time scale τ_k is comparable to the smaller of the two molecular time scales $1/(k^2\nu)$ and $1/(k^2\kappa)$. Consider $Pr \leq 1$, for which the latter is smaller. Substituting earlier results into $\tau_k \sim 1/(k^2\kappa)$, the scaling $Yk_B \sim (RaPr)^{5/16}$ is obtained for the crossover wavenumber k_B , where Ra is based on the length scale Y .

For $Pr \leq 1$, the density spectrum is suppressed at k above k_B by molecular dissipation of density fluctuations. In three-dimensional flow with $Pr < 1$, velocity

fluctuations at k above k_B cascade from wavenumber k_B , at which they are driven by density fluctuations, to a higher- k cutoff at which they are suppressed by viscous dissipation. This cascade is governed by the usual inertial-range dynamics, giving $k^{-5/3}$ scaling of the energy and density spectra in this subrange (Grossmann & L'vov 1993).

In DPE, there is no mechanism other than density fluctuations to drive fluid motions. For k greater than k_B but below the viscous cutoff, scaling analysis of DPE (details omitted) gives $k^{-9/2}$ scaling of the density spectrum. In contrast, for shear-driven stably stratified flow, ODT captures the inertial-range dynamics leading to the $k^{-5/3}$ subrange, for the same reasons that ODT captures this subrange in non-buoyant flow.

For $Pr > 1$, analogous considerations give $Yk_B \sim (Ra/Pr)^{5/16}$, where k_B is now the viscous cutoff. Eddies are suppressed at k above this cutoff, but density fluctuations persist up to a higher wavenumber corresponding to the molecular-diffusive cutoff. The subrange between these cutoffs is a viscous-convective subrange with respect to density, so $1/k$ scaling of the density spectrum is anticipated (Lesieur 1990). DPE as well as shear-driven ODT captures the mechanism that causes this scaling.

For any Pr , eddies and density fluctuations are suppressed at sufficiently high k . Scaling analysis (details omitted) indicates that the high- k falloff of the density spectrum is faster than power law but slower than exponential. This behaviour is qualitatively consistent with current understanding of the far dissipation range (Sirovich *et al.* 1994).

The BO scaling predictions and the predicted scaling of k_B agree with the predictions of L'vov (1991), reflecting the fact that DPE and L'vov's analysis are both predicated on the locality of the buoyancy-driven cascade. Procaccia & Zeitak (1989) derived the BO scaling from a different viewpoint, obtaining a different scaling of k_B . Measurements by Tong & Shen (1992) confirm L'vov's prediction, lending support to the locality principle underlying his analysis and DPE.

These predictions (except Pr dependences) are tested by simulating the imposed-density-gradient configuration with maximum event size Y for two Ra values with $Pr = 1$. Figure 11 shows density spectra (defined in accordance with the scalar spectrum formulation in Appendix B) determined from the statistically steady evolution of this configuration after transient relaxation. The axes are scaled to demonstrate the $Ra^{5/16}$ scaling of k_B . It is seen that the BO spectral scaling and the anticipated Ra dependence of k_B are obeyed. In conjunction with the results of §3, it is thus demonstrated that (2.14) encompasses the physics governing both the inertial cascade and the buoyancy-driven cascade, and thereby provides an opportunity for future study of cascades in mixed convection.

5.2. Rayleigh convection

5.2.1. Heat-transfer analysis

The structure of statistically steady convection between horizontal plates, driven by thermal boundary conditions applied at the plates, is of considerable practical importance and raises scientific issues at the frontier of turbulence research (Siggia 1994). Heat transfer in this flow is the key issue, both from a practical and a fundamental viewpoint. Heat transfer is also a convenient focal point for a general discussion of Rayleigh convection.

Therefore the dependence of the Nusselt number Nu on Ra and Pr is considered, where Nu is the mean heat flux divided by the heat flux in the absence of fluid motion. In statistically steady convection, the mean heat flux is independent of y between the

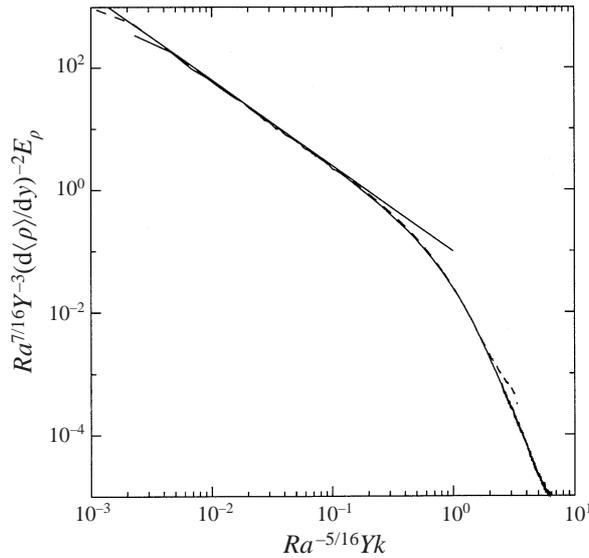


FIGURE 11. Computed power spectra of density fluctuations in stationary homogeneous buoyancy-driven turbulence, normalized to demonstrate the scaling of the high-wavenumber cutoff, for $Pr = 1$: —, $Ra = 10^{11}$; ----, $Ra = 10^{12}$. A line segment of slope $-\frac{7}{5}$ identifies the Bolgiano–Obukhov scaling regime.

plates, so it is equal to $-\kappa d\langle T \rangle / dy|_{y=0}$, the heat flux at the lower plate. (Here, plates are located at $y = 0$ and L . The factor $\rho_0 c$ is omitted because it drops out of all normalized fluxes, assuming constant heat capacity c .) In motionless fluid, $d\langle T \rangle / dy$ is equal to $-\Delta / L$ for all y , where Δ is the magnitude of the imposed temperature difference, and the heat flux is $\kappa \Delta / L$. These relations give

$$Nu = -\frac{L}{\Delta} \left. \frac{d\langle T \rangle}{dy} \right|_{y=0}. \tag{5.1}$$

In DPE, Rayleigh convection is simulated by maintaining an unstable density difference across the y interval $[0, L]$. In the Boussinesq approximation, density and temperature differences are proportional, but opposite in sign, so the thermal interpretation of this configuration follows directly.

In normalized units, this flow is characterized by Ra and Pr . The dependence of Nu on Ra and Pr in DPE is considered. This dependence is sensitive to several features of wall-bounded buoyancy-driven flow in DPE.

The key assumption in the classical similarity analysis of Rayleigh convection is that near-wall flow structure is independent of plate separation L for large Ra . The mixing-length similarity scalings that follow from this assumption explain many features of Rayleigh convection and related flows (Adrian *et al.* 1986; Siggia 1994). However, nonclassical scalings attributed to bulk-flow effects are observed in some high- Ra flow regimes (Siggia 1994).

As in three-dimensional Rayleigh convection, it is anticipated that mixing in the interior of the DPE simulation suppresses the mean density gradient, which therefore resides primarily in conduction-dominated wall layers. This picture is verified self-consistently through scaling analysis, supported by numerical results. The focus of the scaling analysis is estimation of the thickness y_κ of the conduction layers. In particular, the possible dependence of conduction-layer structure on L is considered.

The thickness y_κ is determined by the balance of diffusive broadening of the layers and advective transfer of wall-layer fluid to the interior. Layer broadening and erosion may be visualized as a renewal process in which the layer grows diffusively until advective disruption occurs, followed by regrowth. Diffusive scaling implies $y_\kappa^2 \sim \kappa t_\kappa$, where t_κ is the characteristic disruption time.

Though this picture of successive disruptions is reminiscent of the periodic generation of thermals observed in convection at moderate Ra (Sparrow, Husar & Goldstein 1970), neither the model nor its interpretation relies on a direct correspondence between individual events within the simulation and observed fluid motions. The performance of the model reflects the scalings governing the ensemble of simulated events.

For estimation purposes, a disruption is defined as a mapping of size y_κ or larger whose closest approach to the wall is less than y_κ . Then t_κ is the mean time between such events. In principle, mappings smaller than y_κ may affect the scaling, e.g. through their contribution to an eddy diffusivity $\kappa_e > \kappa$ governing diffusive-layer growth. However, it follows from the ensuing analysis that mappings smaller than y_κ can occur in DPE only if $Pr < 1$, and that κ_e is of order κ in this Pr range.

Thus, large events ($l > y_\kappa$) determine t_κ . Small events ($l < y_\kappa$) enhance diffusive growth of the conductive layer, but not enough to affect scalings.

Consider the mean time $t_\kappa(l)$ between disruptions by mappings of characteristic size $l \geq y_\kappa$. For estimation purposes, each mapping is deemed to redistribute fluid from the zone $[0, y_\kappa]$ uniformly throughout $[0, l]$. (For clarity, the lower layer is considered here.) Therefore (2.15) gives $\Delta E_g \sim g \Delta \rho y_\kappa l$, where $\Delta \rho$ is the imposed density difference across $[0, L]$. (For high Ra , roughly half of this density difference resides within each wall layer.) Equation (2.14) then gives the l -eddy time scale $\tau_l \sim l / \sqrt{g' y_\kappa}$, where g' denotes $g \Delta \rho / \rho_0$.

To express $t_\kappa(l)$ in terms of τ_l , note that (2.2) determines the event-rate distribution λ in terms of l and τ_l . The event rate for order- l eddies with $0 \leq y_0 \leq y_\kappa$ can be estimated by dl -integration of λ over $[l, 2l]$ and dy_0 -integration over $[0, y_\kappa]$. This gives the rate of order- l disruption events, whose inverse is the disruption time scale $t_\kappa(l)$. Thus, $t_\kappa(l) \sim l \tau_l / y_\kappa$, giving $t_\kappa(l) \sim l^2 / \sqrt{g' y_\kappa^3}$.

Now, t_κ is taken to be the smallest $t_\kappa(l)$ such that $l \geq y_\kappa$. In the absence of viscous effects, this gives $t_\kappa = t_\kappa(y_\kappa)$. However, viscosity is implemented in DPE by disallowing events for which $\tau_l > l^2 / (16\nu)$. The smallest allowed event is therefore of size $y_v \sim \nu / \sqrt{g' y_\kappa}$.

It follows from the ensuing solution for y_κ that this minimum size exceeds y_κ only for $Pr > 1$. Therefore $Pr > 1$ and $Pr \leq 1$ are considered separately. (Owing to numerical coefficients omitted from the scalings, the crossover between Pr regimes actually occurs at non-unity Pr ; see § 5.2.2.)

For $Pr > 1$, $t_\kappa = t_\kappa(y_v)$ is evaluated in the relation $y_\kappa^2 \sim \kappa t_\kappa$ to obtain, after some manipulation, $y_\kappa \sim (\kappa \nu^2)^{2/9} / g'^{1/3}$. The estimate $Nu \sim L / y_\kappa$, based on (5.1) and the order- Δ temperature drop in the y_κ -layer, gives

$$Nu \sim Ra^{1/3} Pr^{-1/9}, \quad (5.2)$$

where Ra is given by (2.18).

For $Pr \leq 1$, $t_\kappa = t_\kappa(y_\kappa)$. This gives $y_\kappa \sim (\kappa^2 / g')^{1/3}$ and thus

$$Nu \sim (RaPr)^{1/3}. \quad (5.3)$$

Equations (5.2) and (5.3) necessarily conform to the mixing-length scaling $Nu \sim$

$f(Pr)Ra^{1/3}$, which follows from the assumed insensitivity of near-wall behaviour to L (Siggia 1994). Support for this assumption in the present context is provided shortly.

The Pr dependence in (5.3) is simply a reflection of the irrelevance of the viscosity in the low- Pr limit. The Pr dependence in (5.2) follows from the suppression of fluid motions below the viscous cutoff in DPE. A more complete high- Pr theory that accounts for viscous-scale fluid motions (Kraichnan 1962) gives $Nu \sim Ra^{1/3}$, independent of Pr .

Measurements suggest that neither this result nor (5.2) is entirely accurate. (Kraichnan notes that a key assumption in his theory is unlikely to be strictly correct.) Evidence that Nu is an increasing function of Pr for high Pr is noted shortly.

A corollary of the derivation of (5.2) is the relation $y_v/y_\kappa \sim Pr^{1/3}$ for high Pr . In contrast, Kraichnan's theory predicts that this ratio of viscous-layer and thermal-layer thicknesses scales as $Pr^{1/2}$ for high Pr .

A complication that may affect the Ra as well as the Pr dependence is the occurrence of large-scale interior flows in some high- Ra convection regimes (Siggia 1994). The proposed governing mechanisms involve flow phenomena that are not represented within DPE. Nevertheless, DPE results may have some bearing on measured Nu scalings that have been attributed to these phenomena. Before examining the computed results, large-scale effects in the DPE formulation of Rayleigh convection are analyzed.

Only $Pr > 1$ is considered because all properties of interest are independent of Pr for low Pr . As noted earlier, this insensitivity is shown by comparing κ to the eddy diffusivity κ_e of mappings of size y_κ or less contained within $[0, y_\kappa]$. Straightforward extension of the foregoing analysis gives $\kappa_e \sim y_\kappa^2/\tau_\kappa$, and consequently $\kappa_e \sim \kappa$, for low Pr . This establishes the claimed insensitivity to Pr for low Pr , so only $Pr > 1$ is considered in the remainder of the analysis.

At high Ra , the large-scale flow is characterized by L and the potential energy input rate $Nu \kappa g \Delta \rho / L \sim \kappa g \Delta \rho / y_\kappa$. In steady state, the energy input equals the kinetic energy dissipation rate, of order $\rho_0 v^3 / L$, where v is a characteristic large-scale velocity. This is equivalent to the usual analysis based on the heat flux driven by the imposed temperature difference (Adrian *et al.* 1986), but is more direct for purposes of flow analysis. Then $v \sim (\kappa g' L / y_\kappa)^{1/3}$.

The large-scale flow governs the wall-layer thickness y_κ , and thus Nu , only if it disrupts the wall layer on a time scale shorter than the time scale t_κ determined by considering only the near-wall flow. The large-eddy time scale is $\tau_L \sim L/v$. As in the analysis of wall-layer disruption by size- l eddies, τ_L is multiplied by L/y_κ to obtain the time scale for disruption of the wall layer by large eddies. Combining results thus far, it is found that large-scale flow dominates only for $Ra < Pr^{17/15}$. For given Pr , large-scale effects are negligible at sufficiently high Ra . Thus, DPE does not capture the transition back to large-scale dominance at exceedingly high Ra that was predicted by Kraichnan (1962) and possibly observed in a recent experiment (Chavanne *et al.* 1997).

5.2.2. Heat-transfer results

Rayleigh convection is simulated in DPE by choosing an arbitrary initial density profile, applying constant-density boundary conditions at $y = 0$ and $y = L$ with $\rho(0) < \rho(L)$, and running the simulation until transients are relaxed before gathering statistics. Heat-transfer properties based on simulations performed for various Ra and Pr values are shown in figures 12 and 13.

Figure 12 is scaled so that, for given Pr , (5.2) corresponds to no dependence of the

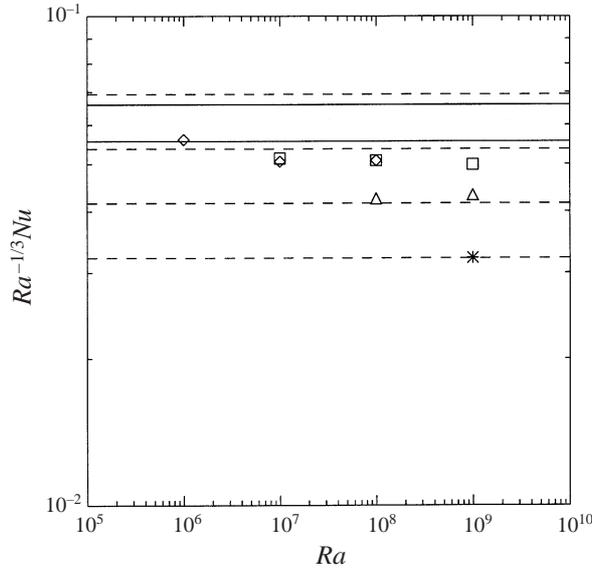


FIGURE 12. Heat transfer in Rayleigh convection, using high- Pr scaling. Computations: \diamond , $Pr = 10$; \square , $Pr = 100$; \triangle , $Pr = 1000$; $*$, $Pr = 10\,000$. Dashed lines are separated by factors of $10^{1/9}$. Measurements: lower solid line, $Pr = 6.5$ (Goldstein & Tokuda 1980); upper solid line, $Pr = 2750$ (Goldstein *et al.* 1990).

plotted quantity on Ra . It is seen that the $Ra^{1/3}$ scaling of Nu is obeyed for $Ra > 10^7$. Results for $Pr = 10, 100, 1000$ and $10\,000$ are shown. The dashed lines are separated by factors of $10^{1/9}$ to indicate the vertical displacement between successive Pr values that is prescribed by (5.2). The anticipated Pr dependence is obtained for $Pr > 100$.

The solid lines represent the $Ra^{1/3}$ scaling of Nu inferred by Goldstein & Tokuda (1980) from measurements at $Pr = 6.5$ (lower line), and by Goldstein, Chiang & See (1990) from measurements at $Pr = 2750$ (upper line). Their results indicate a slight increase of Nu with increasing Pr . Earlier measurements (Globe & Dropkin 1959) indicate the same trend, with stronger Pr dependence ($Nu \sim Pr^{0.074}$). It appears that DPE as presently formulated gives fairly accurate heat-transfer results for Pr of order 10 (corresponding to Rayleigh convection in water), with increasing deviation from measured results as Pr increases.

Results for Pr ranging from 0.01 to 10 are plotted in figure 13. The scaling is chosen so that the data should collapse on a horizontal line if (5.3) is obeyed. The anticipated Pr dependence is seen for Pr below 0.1. High- Ra onset of the anticipated Ra dependence is apparent, though the results are not definitive in this regard.

Figures 12 and 13 indicate that the transition between high- Pr and low- Pr scaling occurs near $Pr = 10$. Experiments, however, indicate that the transition occurs near $Pr = 0.1$ (Siggia 1994). As noted in § 2.4.1, the Pr value in DPE is governed by small-eddy suppression. The suppression criterion involves a somewhat arbitrary numerical factor (Appendix A) that could in principle be adjusted to match the Pr value at which the transition between scalings is observed. Empirical adjustments of this sort are useful for obtaining quantitatively accurate, calibrated models of particular flows, but are not attempted here.

In the DPE results and in measurements, transitional Ra dependences of Nu are seen for Pr of order unity or less. Summarizing their own and previous measurements,

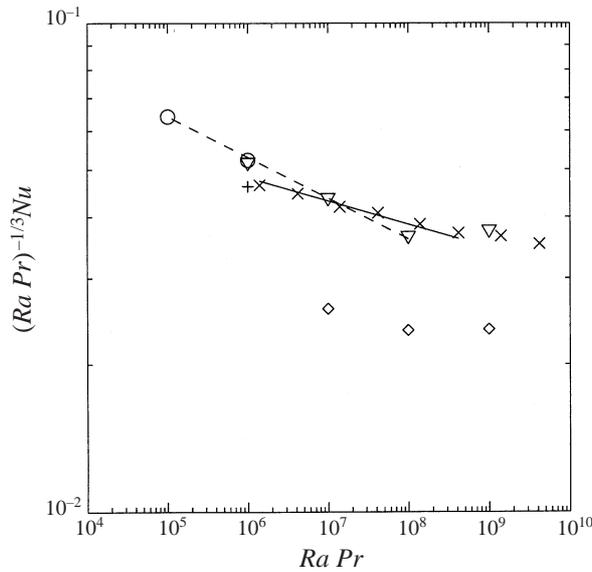


FIGURE 13. Heat transfer in Rayleigh convection, using low- Pr scaling. Computations: \circ , $Pr = 0.01$; ∇ , $Pr = 0.1$; \times , $Pr = 0.7$; $+$, $Pr = 1$; \diamond , $Pr = 10$. Line segments: -----, $Nu \sim Ra^{1/4}$; ———, $Nu \sim Ra^{2/7}$.

Cioni, Ciliberto & Sommeria (1997) conclude that the power of Ra appearing in the Nu scaling is 0.26 at low Pr , near $\frac{2}{7}$ at Pr of order unity, and near $\frac{1}{3}$ at high Pr . Large-scale motions are observed that depend on vessel shape and on Pr , but at Pr of order unity, the suppression of these motions by screens does not change the heat-transfer scaling.

Cioni *et al.* (1997) note the difficulty of reconciling these and other observations with various models that have been proposed. The models typically involve the application of mixing-length concepts to a proposed schematic picture of the flow. The models for different regimes bear no obvious relation to each other.

It is interesting in this regard that DPE exhibits significant (two decades or longer) transitional Nu scalings that are consistent with the 0.26 and $\frac{2}{7}$ exponents seen at low and moderate Pr respectively. Also consistent with measurements is the robustness of $Ra^{1/3}$ scaling at high Pr . The DPE results for low Pr are especially interesting because they indicate $Nu \sim Ra^{1/4}$ transitional scaling and also indicate a Re scaling that is consistent with measurements (§ 5.2.4). In contrast, a low- Pr mixing-length analysis that reproduces $Nu \sim Ra^{1/4}$ scaling disagrees with the measured Re scaling (Cioni *et al.* 1997).

Thus, DPE reconciles a variety of behaviours that have not previously been explained within a single framework. Application of mixing-length analysis to DPE itself does not explain the performance of the model. As shown in § 5.2.1, $Nu \sim Ra^{1/3}$ is predicted for all Pr regimes of the DPE simulation. The additional transitional scalings seen in the DPE numerical results highlight the distinction between conventional mixing-length analysis and mixing-length physics as embodied in DPE (or more generally, in ODT). Equation (2.3) is a mixing-length relation applied to an individual eddy, rather than to an ensemble-averaged flow property. Owing to the strong two-way coupling between mapping events and the velocity profile, this formulation admits the possibility of flow evolution qualitatively different from

the evolution predicted by conventional mixing-length analysis applied to ensemble-averaged properties. The agreement between the heat-transfer regimes of DPE and measured behaviours suggests that DPE does in fact capture physics not described by conventional mixing-length analysis. The simplicity of the model suggests that the relevant physics is not specific to boundary-layer structure, large-scale flow, or plume development, all of which have been proposed as possible governing mechanisms (Siggia 1994; Cioni *et al.* 1997).

5.2.3. Thermal structure

Profiles of moments of the temperature profile in Rayleigh convection have been obtained for $Pr = 0.7$ from DNS (Kerr 1996). Analogous profiles are obtained from DPE simulations which have been performed for Ra and Pr values corresponding to those of the DNS study. DPE and DNS values of scaling exponents governing the Ra dependence of features of these profiles are compared.

Following Kerr (1996), the structure of the temperature variance profile is characterized by Δ_c/Δ , Δ_w/Δ , and λ_T/L , where Δ_c is the centerline r.m.s. temperature fluctuation, Δ_w is the peak r.m.s. fluctuation, and λ_T is the distance of the peak from the wall. Classical mixing-length theory predicts $\Delta_c \sim Ra^{-1/9}$ and $\lambda_T \sim Ra^{-1/3}$, but an alternative mixing-length analysis predicts $\Delta_c \sim Ra^{-1/7}$ and $\lambda_T \sim Ra^{-2/7}$ (Castaing *et al.* 1989). DPE obeys both classical scalings although it obeys a non-classical Nu scaling in this parameter range (§5.2.2). The DNS results (Kerr 1996) do not clearly discriminate between the classical and non-classical scalings. Both DPE and DNS indicate that Δ_w decreases more slowly with Ra than Δ_c . Collectively, the thermal-structure and heat-transfer results indicate various transitional behaviours that are not readily subsumed within a conventional mixing-length picture.

5.2.4. Flow properties

The principal characterization of flow as distinct from thermal properties of Rayleigh convection is the Reynolds number $Re = vL/\nu$, where the characteristic velocity v is taken to be the r.m.s. vertical velocity fluctuation $\langle v^2 \rangle^{1/2}$ midway between the walls. The parametric dependences of Re are estimated using conventional mixing-length theory. It is assumed that the energy dissipation, of order $\rho_0 v^3/L$, is proportional to the potential energy input rate $Nu \kappa g \Delta \rho / L$. This gives the mixing-length prediction (Siggia 1994)

$$Re \sim (NuRa/Pr^2)^{1/3} \quad (5.4)$$

for all Pr .

This relation is expressed in terms of Nu , rather than substituting a particular dependence of Nu on Ra and Pr , so that it may in principle subsume all Nu scaling regimes. However, the scaling $\rho_0 v^3/L$ assumed for the energy dissipation may not be applicable if the dissipation is governed by the interaction between a large-scale interior flow and the wall layer. Siggia (1994) shows that near-sidewall velocity measurements for Pr near unity deviate from (5.4) in a manner that suggests such an interaction.

DPE lacks the mechanism that causes this deviation. Accordingly, figure 14 shows that the DPE results obey (5.4) over the entire range of Pr and Ra spanned by the simulations, except for possible low- Re deviations.

Also plotted in figure 14 are experimental and numerical data correlations. The DNS results of Kerr (1996) for $Pr = 0.7$ suggest a departure from the Ra dependence

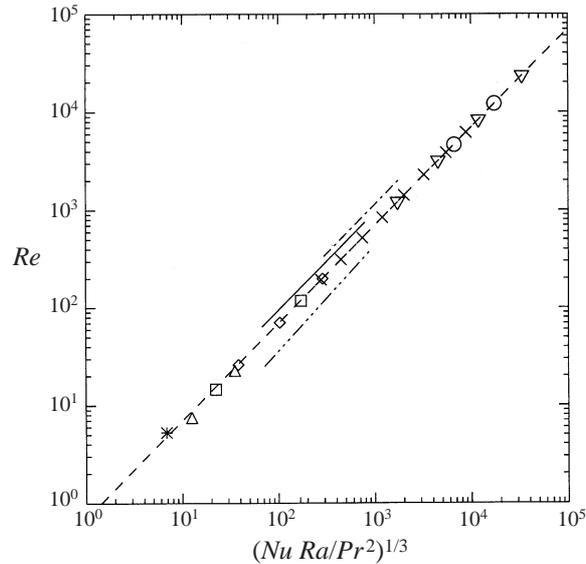


FIGURE 14. Computed Re in coordinates based on mixing-length theory. Symbols as in figures 12 and 13; ----, linear fit to computed results. Correlations inferred from measurements: —, $Pr = 0.7$ (Fitzjarrald 1976); - · -, $Pr = 7$ (Tanaka & Miyata 1980). - · · · -, correlation based on direct numerical simulation for $Pr = 0.7$ (Kerr 1996). Correlations are plotted over the ranges of the respective data sets.

implied by (5.4), but interior-flow velocity measurements for $Pr = 0.7$ (Fitzjarrald 1976) and $Pr = 7$ (Tanaka & Miyata 1980) obey that Ra dependence. The $Pr = 7$ result is obtained by assuming isotropy of the interior flow. The accuracy of this assumption was not checked, so the difference between the two measured correlations does not necessarily imply a deviation from the Pr dependence of (5.4). A flow Reynolds number inferred from thermal time histories has also been found to obey (5.4) for given Pr (Cioni *et al.* 1997). The ODT results and the comparisons to DNS and experimental results indicate that the definition of velocity in terms of the cell displacement and the event time scale in § 2.4.1 is consistent with the classical mixing-length theory of Rayleigh convection and yields reasonably accurate quantitative results.

5.3. Penetrative convection

A key feature of atmospheric-boundary-layer (ABL) dynamics is the daytime growth of the buoyancy-driven mixed layer as it penetrates the stably stratified layer established earlier by nocturnal surface cooling (Stull 1988). Deardorff's (1970) convective scalings have been used to correlate a variety of laboratory and field measurements and numerical simulations of mixed-layer structure (Adrian *et al.* 1986; Coleman & Ferziger 1996). The correlations indicate that important features of the scaled structure are insensitive to Reynolds number, mean shear, Coriolis effects, and transient growth of the layer.

Deardorff & Willis (1985) performed a shear-free penetrative-convection experiment that has become a benchmark for mixed-layer data correlations. Their configuration is an initially linear, stable thermal stratification, heated from below.

In DPE, this configuration is simulated by applying a constant density flux $-Q$ at the bottom of a linear, stable initial density profile characterized by the length scale

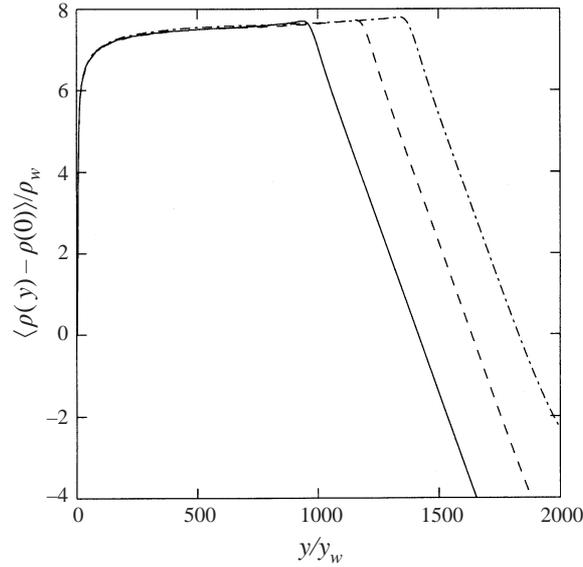


FIGURE 15. Computed mean density profiles in penetrative convection, referenced to the density at the wall, in wall coordinates, for $Pr = 6$, $Re_m = 1544$ (—), 2044 (----), and 2488 (-·-).

$L \equiv \rho_0 / (d\rho/dz)$. Computed results are normalized using either wall-layer (conduction) scalings

$$v_w = (g\kappa Q / \rho_0)^{1/4}, \quad y_w = \kappa / v_w, \quad \rho_w = Q / v_w \quad (5.5)$$

or mixed-layer (convection) scalings

$$y_m, \quad v_m = (gy_m Q / \rho_0)^{1/3}, \quad \rho_m = Q / v_m, \quad (5.6)$$

where y_m is a measure of mixed-layer depth (Adrian *et al.* 1986). The mixed-layer flow is characterized by Pr and the Reynolds number $Re_m = v_m y_m / \nu$. Computations were performed for $Pr = 6$, corresponding to the experimental conditions of Deardorff & Willis (1985), and also for $Pr = 1$. Flow evolution was simulated until $Re_m = 2500$ was reached. Coleman & Ferziger (1996) estimated that the typical Re_m value for the Deardorff–Willis experiment was 2000.

The collapse of conduction-scaled mean density profiles obtained from the $Pr = 6$ simulations is shown in figure 15. A slight unstable stratification is seen in the mixed layer, but Deardorff & Willis (1985) obtained a slight stable stratification.

Away from the conduction layer, collapse of convection-scaled quantities is obtained for Re_m above 1200, with one exception that is noted shortly. Plotted profiles correspond to Re_m in the vicinity of 2000.

The scaled flux profiles (density flux for the simulation, heat flux for the experiment) shown in figure 16 indicate almost uniform heating of the mixed layer, owing to the suppression of thermal gradients by turbulent transport. The profiles show flux reversal above the mixed layer, reflecting entrainment of fluid from the stable capping layer. The mixed-layer depth y_m is defined as the y location of the most negative flux (Deardorff, Willis & Stockton 1980).

The experiment indicates stronger flux reversal than the simulation. To assess how this affects the growth rate of the mixed layer, it is important to distinguish between entrainment and encroachment (Turner 1991). Encroachment is growth of

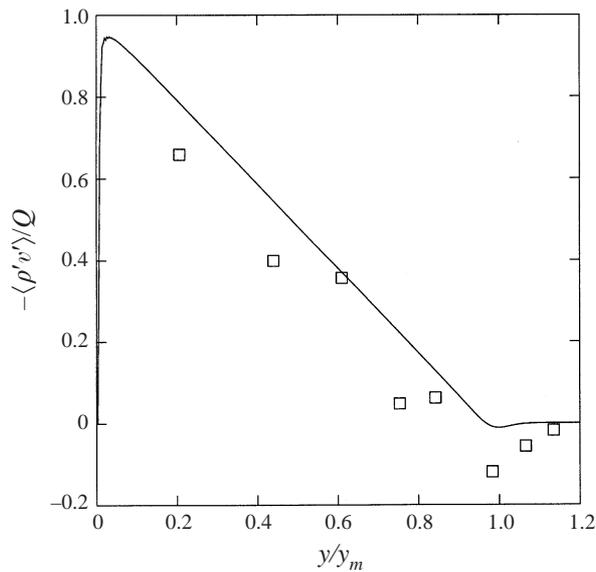


FIGURE 16. Computed (—) and measured (Deardorff & Willis 1985; symbols) vertical profiles of density flux, normalized by its wall value, for $Pr = 6$. (Measured profile is the thermal analogue of this quantity.)

the near-constant-property layer caused by the influx of the conserved property at the boundary, irrespective of advection within the layer.

A simple model of this process is obtained by assuming that ρ is independent of y in the mixed layer $y < y_m$ and has its initial, linear functional form for $y > y_m$. For constant Q , this yields $t^{1/2}$ growth of y_m . The predicted growth is found to be in good numerical agreement with the computed evolution of y_m . Analogous reasoning led Deardorff, Willis & Lilly (1969) to a good prediction of mixed-layer growth in their penetrative convection experiment. Thus, encroachment rather than advective entrainment appears to be the dominant growth process in this shear-free flow configuration, so differences between computed and observed rates of advective entrainment have little impact on the overall growth rate.

The simplicity of this picture of mixed-layer growth is specific to penetrative convection. Shear-driven entrainment involves additional considerations that are examined in § 6.3.

In figure 17, computed density-fluctuation profiles are compared to temperature fluctuations measured by Deardorff & Willis (1985). The computed $Pr = 6$ profile, corresponding to measurement conditions, reproduces the observed features, including the fluctuation enhancement above the mixed layer caused by entrainment of upper-layer fluid. Significant Pr dependence of this feature is seen, suggesting that fluctuations in the entrainment zone may be governed by a local Reynolds number that is much smaller than Re_m . Significant Re_m dependence of this feature is also found throughout the Re_m range of the computations. Values of Re_m much larger than those of the experiment and the computations may be needed to obtain complete mixed-layer similarity. This may partly explain the difference between laboratory and field measurements of temperature fluctuations in the entrainment zone of penetrative convection, although the field measurements involve other complications that preclude a definitive interpretation (Deardorff & Willis 1985).

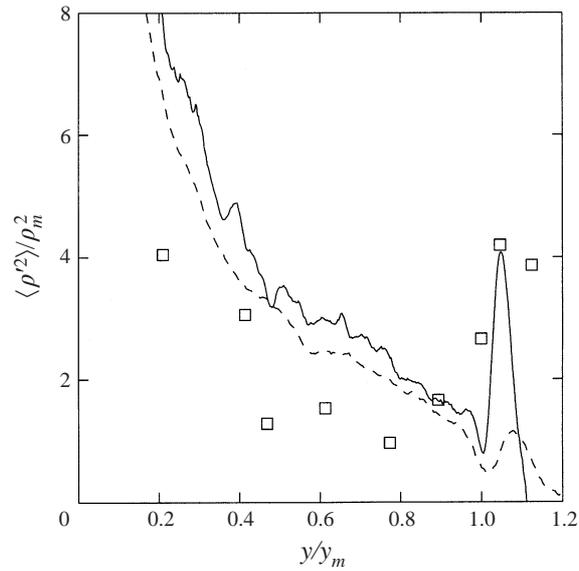


FIGURE 17. Vertical profiles of density variance, normalized by the convective density scale, plotted as in figure 16. A profile computed for $Pr = 1$ is also shown (-----).

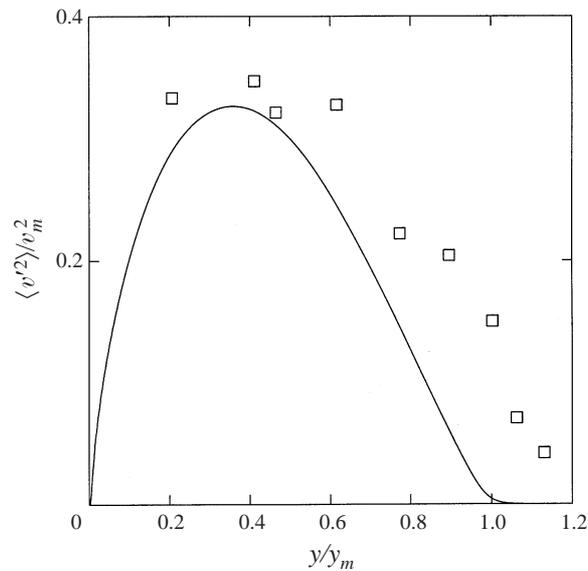


FIGURE 18. Vertical profiles of vertical-velocity variance, normalized by the convective velocity scale, plotted as in figure 16.

Computed vertical-velocity variance profiles for Re_m above 1200 exhibit mixed-layer collapse with no significant Pr sensitivity. A representative profile, shown in figure 18, agrees with the measured peak but falls off too rapidly above the mixed layer. This discrepancy may reflect the absence of wave phenomena in the model. It has been proposed that impingement of turbulent eddies on the stable layer induces internal waves in that layer that induce property fluctuations in and above the entrainment zone (Townsend 1964). The absence of this effect in the model may not be a major

shortcoming because internal waves are unlikely to enhance mixing unless they break. Moreover, figure 17 indicates that the model captures the temperature fluctuations associated with entrainment.

Several second-order closure methods (Lumley, Zeman & Siess 1978; Mellor & Yamada 1982) reproduce the principal features of penetrative convection, albeit with considerable empiricism not required by DPE. Those studies reach different conclusions concerning the mechanistic basis of model performance. Clarification might be provided by application of the same formulations to Rayleigh convection. Application of second-order closure to Rayleigh convection has not yet been reported, although other closure methods have been applied to this flow (Hanjalić & Vasić 1993; Hanjalić, Kenjereš & Durst 1996; Canuto, Dubovikov & Dienstfrey 1997).

6. Stratified boundary layers

6.1. Monin–Obukhov similarity

The atmospheric boundary layer is the principal motivation for the study of buoyant stratified boundary layers. Some laboratory results have been obtained (Rey, Schon & Mathieu 1979), but ABL field measurements are the main source of information on this class of flows. In particular, field studies are the main source of support for Monin–Obukhov (MO) similarity (Kaimal & Finnigan 1994). This similarity hypothesis states that certain near-wall flow properties scaled by wall parameters are universal functions of y/L , where the Obukhov length

$$L = \frac{\rho_0 u_\tau^3}{\kappa_V g F_\rho} \quad (6.1)$$

(here expressed in terms of density flux F_ρ rather than the usual temperature formulation) governs the transition from near-wall shear dominance to far-field buoyancy dominance in stratified boundary layers. L is positive (negative) for stable (unstable) stratification.

In terms of u_τ and $T_0 \equiv -F_\theta/u_\tau$, where F_θ is the surface temperature flux, MO similarity is obtained for the following quantities:

$$\phi_m = \frac{\kappa_V y}{u_\tau} \frac{d\langle u \rangle}{dy}, \quad (6.2)$$

$$\phi_h = \frac{\kappa_V y}{T_0} \frac{d\langle \theta \rangle}{dy}, \quad (6.3)$$

$$\phi_v = \frac{\langle v'^2 \rangle^{1/2}}{u_\tau}, \quad (6.4)$$

$$\phi_\theta = \frac{\langle \theta'^2 \rangle^{1/2}}{|T_0|}, \quad (6.5)$$

$$\phi_\epsilon = \frac{\kappa_V y \epsilon}{u_\tau^3}, \quad (6.6)$$

$$r_{uw} = \frac{\langle u'v' \rangle}{\langle u'^2 \rangle^{1/2} \langle v'^2 \rangle^{1/2}}, \quad (6.7)$$

$$r_{\theta v} = \frac{\langle \theta'v' \rangle}{\langle \theta'^2 \rangle^{1/2} \langle v'^2 \rangle^{1/2}}, \quad (6.8)$$

insofar as the ABL data allow a determination. Despite the apparent MO similarity of r_{uv} , horizontal velocity fluctuations have been found to exhibit deviations from MO similarity. This has been explained on the basis of bulk motions, scaling with the convective-layer thickness, that are primarily vertical in the bulk but are deflected horizontally near the wall (Yaglom 1994).

The following empirical similarity functions have been obtained for unstable stratification in the y range $-2L \leq y \leq 0$:

$$\phi_m = (1 + 16|y/L|)^{-1/4}, \quad (6.9)$$

$$\phi_h = (1 + 16|y/L|)^{-1/2}, \quad (6.10)$$

$$\phi_v = 1.25(1 + 3|y/L|)^{1/3}, \quad (6.11)$$

$$\phi_\theta = 2(1 + 9.5|y/L|)^{-1/3}, \quad (6.12)$$

$$\phi_\epsilon = (1 + 0.5|y/L|^{2/3})^{3/2}. \quad (6.13)$$

For stable stratification in the y range $0 \leq y \leq L$, the empirical similarity functions

$$\phi_m = \phi_h = \phi_\epsilon = 1 + 5y/L, \quad (6.14)$$

$$\phi_v = 1.25(1 + 0.2y/L)^{1/3}, \quad (6.15)$$

$$\phi_\theta = 2(1 + 0.5y/L)^{-1}, \quad (6.16)$$

have been obtained. The measured correlations are $r_{uv} = -0.35$ ($-L < y < L$), $r_{\theta v} = 0.5$ ($-2L < y < 0$) and $r_{\theta v} = -0.4$ ($0 < y < L$). These are the functional forms reported by Kaimal & Finnigan (1994), except for (6.15), which is an updated result (Kaimal 1996, personal communication).

ODT exhibits MO similarity of the quantities (6.2)–(6.8), and also of the quantity $\phi_u = \langle u^2 \rangle^{1/2}/u_\tau$ that does not obey MO similarity in the ABL. The latter artifact reflects the absence of pressure effects that deflect vertical motions horizontally. In ODT, $u(y)$ is a scalar field rather than a component of a vector field.

In figure 19, the empirical similarity functions (6.9)–(6.16) are compared to ODT simulations of statistically stationary Couette flow (as in §4), with density stratification introduced by maintaining a density difference $\Delta\rho$ across the flow domain $[0, Y]$. Couette flow is chosen because the constant-density simulation (§4) exhibits a substantial logarithmic range of $u(y)$, as required for MO similarity, at moderate Re . Density statistics are interpreted as temperature statistics, as explained in §2.4.1. Computed results for ϕ_h are not shown because they are almost indistinguishable from computed results for ϕ_m . (Because u is a scalar field in ODT, computed results for these two quantities are equivalent for this configuration if $Pr = 1$; the two differ slightly in the present computations because the value $Pr = 0.7$ corresponding to ambient air was adopted.) For each stratification, computed results are shown for several conditions, parameterized by $Ri = gY\Delta\rho/(\rho_0U^2)$, in order to demonstrate MO similarity. (Here, negative Ri corresponds to unstable stratification.)

Owing to ill-defined boundary conditions at the Earth's surface, the ODT parameter A is not assigned on the basis of earlier comparisons to laboratory flows. Rather, it is chosen to give the best fit to the MO similarity functions determined from ABL measurements. The computed similarity functions ϕ_m , ϕ_h , and ϕ_ϵ for the stable ABL are far more sensitive to A than any of the others, so in effect A is chosen to fit these functions to the empirical correlation (6.14). On this basis, the value $A = 0.33$ is assigned.

MO similarity is applicable above the viscous sublayer but below the y range

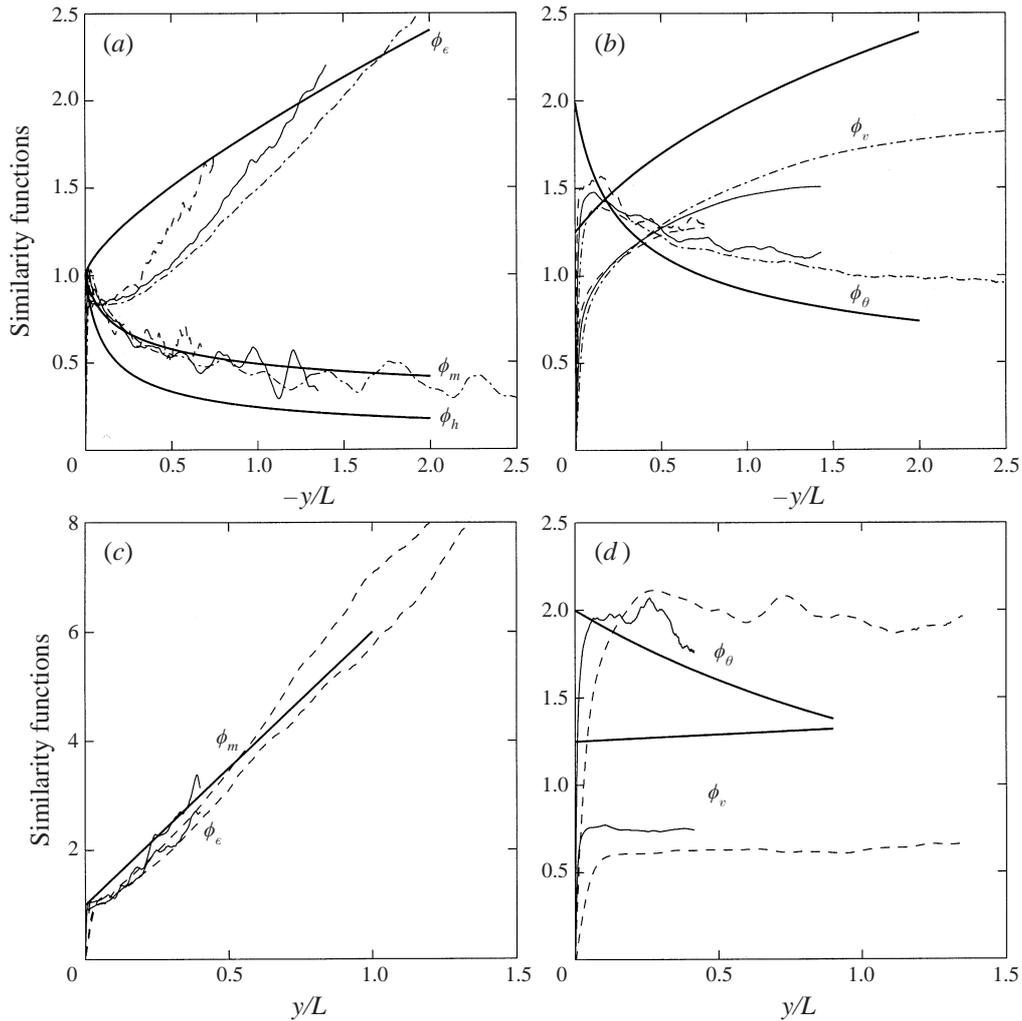


FIGURE 19. Monin-Obukhov similarity functions for stratified boundary layers. $Re = 12\,500$ for all computed cases (based on $A = 0.33$). Computations: $Ri = -1.25$ (-----), -2.5 (—), -5 (---), 0.5 (——), 1 (----). Thick curves are empirical similarity functions (Kaimal & Finnigan 1994; Kaimal 1996, personal communication). (a) Computed and empirical similarity functions ϕ_ϵ (higher curves) and ϕ_m (lower curves) for unstable stratification ($Ri < 0$). The empirical function ϕ_h is also shown. (b) Computed and empirical similarity functions ϕ_v (upward-trending curves) and ϕ_θ (downward-trending curves) for unstable stratification. (c) Computed similarity functions ϕ_m (higher curves) and ϕ_ϵ (lower curves) for stable stratification ($Ri > 0$). Empirical functions for the quantities ϕ_m , ϕ_h and ϕ_ϵ are identical (thick curve). (d) Computed and empirical similarity functions ϕ_θ (higher curves) and ϕ_v (lower curves) for stable stratification.

subject to outer-flow effects such as mixed-layer scaling. The correlations of ABL field data are extrapolations to $y = 0$, reflecting the very high Re of the ABL. The computations, performed at moderate Re , exhibit viscous-sublayer behaviour, and consequent deviation from MO similarity, for y/L below 0.1. Deviation of some, but not all, computed similarity functions is seen at large y . Apart from these anticipated deviations, conformance to MO similarity is evident for all quantities, with the possible exception of ϕ_ϵ in unstable stratification. It is unclear whether this quantity deviates

from MO similarity or whether the apparent deviations are due to especially high sensitivity to outer-flow effects.

For stable stratification, the computed functions ϕ_m , ϕ_h , and ϕ_ϵ are roughly linear in y , and ϕ_v and ϕ_θ are roughly constant in y , except at small y/L . These behaviours correspond to constancy in y of the quantities $d\langle u \rangle/dy$, $d\langle \theta \rangle/dy$, $\langle v^2 \rangle$, $\langle \theta^2 \rangle$ and ϵ . In this flow, the energetically allowed eddies that govern local properties are smaller than the distance to the wall layer, so local properties interact with the viscous sublayer only through the gradients $d\langle u \rangle/dy$ and $d\langle \theta \rangle/dy$. This behaviour is the model analogue of the ‘z-less’ scaling (Stull 1988) seen in the stably stratified ABL. (z is the conventional notation for the vertical coordinate in the geophysics literature.)

Computed correlations are roughly constant in y , as indicated by measurements, with computed values $r_{\theta v} = -r_{wv} = 0.6$ for unstable stratification and $r_{\theta v} = r_{wv} = -0.6$ for stable stratification. ODT does not capture the measured differences between the magnitudes of $r_{\theta v}$ and r_{wv} for the same reason that it does not capture the difference between ϕ_m and ϕ_h .

6.2. Implications for atmospheric-boundary-layer modelling

Closure modelling has yielded good predictions of the principal MO similarity functions, based on formulations involving various degrees of empiricism (Mellor & Yamada 1982; Tsarenko 1989). Moreover, closure modelling is directly applicable to the transient evolution of the ABL, but the requisite parameter adjustments become somewhat arbitrary in some instances (Mellor & Yamada 1982; Stull 1988; Zhang & Stull 1992).

Though there are some significant differences between computed and measured MO similarity functions, it is evident that ODT provides a model of the ABL that is sufficiently quantitative for many purposes. ODT simulation of the ABL would require less empiricism than closure models, yet would provide a mechanistically more literal representation of transient phenomena. The stochastic nature of the simulation allows the generation of multiple realizations for given initial and boundary conditions, allowing an estimate of the degree of predictability of a particular transient as well as an estimate of its ensemble-mean behaviour. In contrast, closures predict mean behaviour whose relation to a particular field measurement may not be readily apparent. Parameter adjustment in this context is particularly problematic.

For ABL applications, ODT cannot provide full resolution of the shear-dominated surface layer in a simulation that spans the entire ABL. One possible approach would be to run simulations at lower resolution, using an eddy viscosity (as in three-dimensional large-eddy simulations) to represent the unresolved scales. This formulation might be used as a boundary-layer subgrid model in large-scale circulation models that do not resolve the ABL. ODT might capture ABL transients not represented by parameterized average properties. Alternatively, ODT might be used to develop or test parameterizations of mixed-layer growth and related localized phenomena (Stull 1988).

6.3. Shear-driven entrainment

Entrainment of quiescent, stably stratified fluid into a turbulent mixed zone is an important feature of geophysical flows. Buoyancy-driven entrainment, a key ABL growth mechanism, has been considered in §5.3. Shear-driven entrainment occurs in many contexts (Fernando 1991). Wind shear drives turbulence that deepens the upper-ocean mixed layer, and in some circumstances is the dominant growth mechanism of the ABL.

It was noted that mixed-layer growth in penetrative convection is dominated by the encroachment mechanism, governed by the influx of a conserved property. The turbulent kinetic energy produced by applied shear is not a conserved quantity, owing to viscous dissipation and possible conversion to internal-wave energy. Therefore the parameterization of shear-driven entrainment is based on postulated scalings rather than exact relations.

Several different parameterizations have been proposed, reflecting the abundance of dimensional quantities characterizing the flows of interest (Fernando 1991). For a given parameterization, different experiments indicate different functional dependences, reflecting the absence of a unifying principle. A rough empirical correlation is obtained by plotting u_e/U versus Ri_U , where u_e is the entrainment velocity, U is the velocity jump across the interface, and $Ri_U = g\Delta\rho h/(\rho_0 U^2)$ is the overall Richardson number based on U , the thickness h of the mixed layer, and the density jump $\Delta\rho$ across the interface (Fernando 1991). Computed results presented here are compared to functional dependences proposed by Christodoulou (1986) based on this parameterization.

The simulated flow is a planar boundary layer in the domain $y \geq 0$ with the initial and boundary conditions $u(y, 0) = 0$ and $u(0, t) = U_0$. As in most studies of shear-driven entrainment, the coordinate system is chosen so that the shear-free fluid at large y is at rest. A stable, linear initial density profile is imposed, characterized by the length scale $L = \rho_0/|d\rho/dy|$.

This flow is chosen because it is simple (governed by the buoyant-to-advective time-scale ratio $\Omega = (U_0^2/\nu)\sqrt{L/g}$ and Pr), it spans a relatively wide range of Ri_U in each simulation, and it is analogous to the penetrative convection simulation of § 3.4. In both flows, a stable, linear density profile is destabilized by a flux applied at $y = 0$ (density flux for penetrative convection, momentum flux for shear-driven entrainment).

No experiment performed to date corresponds precisely to this flow configuration. The present objective is to compare computed results to empirical correlations reflecting diverse experimental results.

For this flow, the parameter A in (2.14) is determined by invoking a mathematical stability criterion for shear-driven entrainment. Unbounded parallel shear flows are stable to infinitesimal disturbances when the gradient Richardson number $Ri_g = -(g/\rho_0)(d\rho/dy)/(du/dy)^2$ exceeds $\frac{1}{4}$ (Fernando 1991). The ODT analogue of this marginal stability criterion is obtained by setting the right-hand side of (2.14) equal to zero. Assuming linear profiles of ρ and u , Δu in (2.14) is equal to $l|du/dy|$ for a size- l mapping, based on (2.4) and (2.5). For a size- l mapping of a linear density profile, (2.15) gives $\Delta E_g = \frac{2}{27}gl^3|d\rho/dy|$. Combining these results, the marginal stability criterion for ODT becomes $Ri_g = A^2$. The criterion $Ri_g = \frac{1}{4}$ then gives $A = 0.5$. This value of A is adopted for shear-flow entrainment simulations, so this application requires no empirical input.

This reasoning is not meant to imply that ODT accurately represents the flow instability mechanism. Rather, the choice $A = 0.5$ forces the ODT instability threshold to be consistent with the mathematically prescribed threshold. (See § 2.5 for further discussion of parameter evaluation.)

Runs were performed for $\Omega = 4500$, 10 000, and 31 600, respectively, for $Pr = 0.7$. These computations span three decades of Ri_U . Results discussed shortly indicate that mean-flow evolution is insensitive to Ω . (Fluctuation properties of this flow are not considered here.) The purpose of varying Ω is to vary the range of Ri_U covered

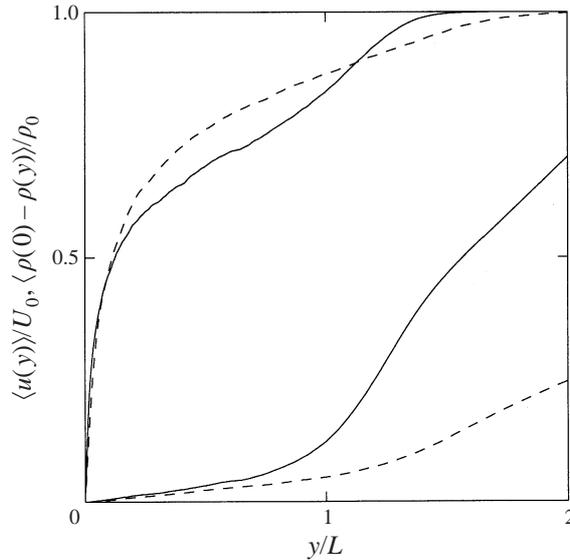


FIGURE 20. Computed mean profiles of velocity (higher curves) and density (lower curves) in shear-driven entrainment with an initially linear stable density profile, $\Omega = 10000$. Profiles plotted for $Ri_U = 0.02$ (-----) and 0.2 (—).

in each run. A more comprehensive sensitivity study, including fluctuation properties, would be of interest, but the present objective is a limited initial study of the mean entrainment rate.

The quantities U , h , and $\Delta\rho$ are defined in a manner that allows consistent comparison to other flows. Following Ellison & Turner (1959), the definitions

$$U = \int \langle u \rangle^2 dy / \int \langle u \rangle dy \quad (6.17)$$

and

$$h = (1/U) \int \langle u \rangle dy \quad (6.18)$$

are adopted. Their definition of $\Delta\rho$ is specific to flows that have constant density in the shear-free zone, so the more generally applicable formulation of Kato & Phillips (1969) is adopted. Namely, the initial density profile is averaged over $0 \leq y \leq h$ and this average is subtracted from the initial density at $y = h$. In effect, the density profile is modelled as a perfectly mixed layer abutting a region unaffected by mixing (or by molecular diffusion). For a linear initial profile, this gives

$$\Delta\rho = \rho_0 h / (2L). \quad (6.19)$$

Figure 20 shows computed mean profiles of u and ρ for two Ri_U values. As Ri_U increases, the profiles develop shoulders in the region of transition from the mixed zone to the stable outer zone. Experiments indicate analogous behaviour.

Figure 21 shows u_e/U plotted as a function of Ri_U , where $u_e = dh/dt$ is the entrainment velocity. Where results for different Ω values overlap, no noticeable sensitivity to Ω is seen.

Solid line segments are empirical correlations developed by Christodoulou (1986). The slopes are based on various proposed scaling regimes of shear-driven entrainment.

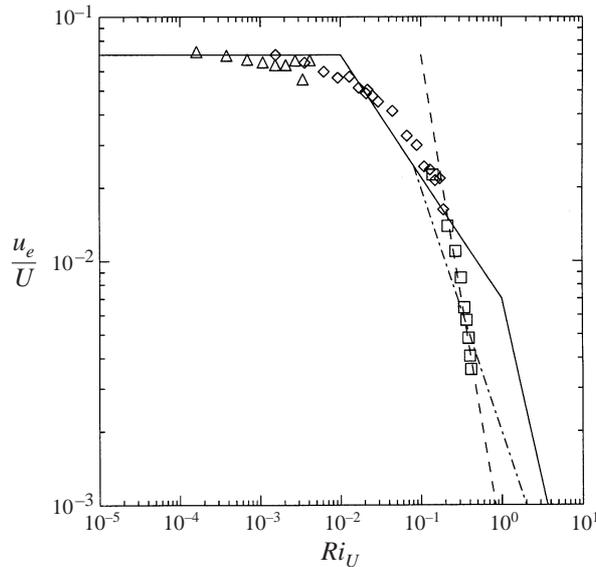


FIGURE 21. Normalized entrainment velocity u_e/U versus Ri_U , computed for $\Omega = 4500$ (\square), 10 000 (\diamond), and 31 600 (\triangle). Lines: empirical correlations (Christodoulou 1986), slopes 0, $-\frac{1}{2}$, and $-\frac{3}{2}$ (—); proposed intermediate scaling, slope -1 (---); presumed high- Ri_U asymptote of the model, slope -2 (-·-·-).

The scatter of measured u_e/U values for different flow configurations is typically an order of magnitude for given Ri_U . Within this scatter, it is not possible to discriminate whether there is an intermediate Ri_U^{-1} range between the $Ri_U^{-1/2}$ and $Ri_U^{-3/2}$ ranges. In fact, the aggregate data do not convincingly support any power-law scaling. (More convincing power-law regimes have been obtained from grid-turbulence experiments involving no mean shear; see Turner 1973. In the absence of mean shear, U is taken to be a measure of turbulence intensity.)

Owing to the experimental scatter, the agreement between the computed results and the empirical correlation must be interpreted carefully. The level of the horizontal line is based on the measured spreading rate of constant-density turbulent jets, as interpreted in this context by Ellison & Turner (1959). The computed result is based on an A value determined by a buoyancy criterion, so the agreement with constant-density flow behaviour may be fortuitous.

Deviation from constant u_e/U indicates buoyant suppression of entrainment. An eventual transition to Ri_U^{-2} falloff is anticipated, based on the following eddy-diffusivity picture of shear-driven entrainment in ODT. The turbulent diffusivity in the mixed layer is of order Uh . This gives $dh^2/dt \sim Uh$, and thus $u_e \sim U$, if buoyant suppression is absent. Consider the modification of this relation caused by buoyant suppression at high Ri_U . Order- h eddies are assumed to dominate the entrainment, but their maximum penetration beyond the mixed layer, denoted δ , is assumed to be much less than h . Eddies that would penetrate farther than δ yield a negative value on the right-hand side of (2.14), and hence do not occur. This reduces the frequency of penetrating eddies by a factor of order δ/h relative to their frequency in the absence of buoyant suppression. With buoyant suppression, the mixed-layer growth per penetrating eddy is of order δ rather than order h , contributing an additional factor of δ/h . Thus, $u_e/U \sim (\delta/h)^2$ at high Ri_U .

The maximum penetration, δ , is estimated by setting the right-hand side of (2.14) equal to zero and substituting the estimates $\Delta u \sim U$, $l \sim h$, and $\Delta E_g \sim g\Delta\rho h\delta$. The last estimate is based on the order- h downward displacement of a fluid parcel of width δ that is less dense, by an amount $\Delta\rho$, than the mixed-layer fluid. The result is $\delta/h \sim Ri_U^{-1}$.

Based on this estimate, the high- Ri_U scaling $u_e/U \sim Ri_U^{-2}$ is obtained. This is a faster falloff than the $Ri_U^{-3/2}$ scaling that is seen experimentally, and that has been interpreted in terms of instability mechanisms at strongly stabilized interfaces (Fernando 1991). ODT omits two phenomena that promote high- Ri_U entrainment: internal-wave formation and breaking, and eddy distortion at the interface. (Buoyancy affects the eddy time scale in ODT, but it does not change the functional form of the triplet map.)

The dimensional analysis underlying the model formulation may nevertheless be physically relevant. The Ri_U^{-2} scaling may be a lower bound on the high- Ri_U falloff. In turbulent entrainment with no mean shear, Ri_U^{-2} falloff has been reported, though slower falloff is more common (Fernando 1991).

Figure 21 indicates that the ODT falloff may in fact be steeper than Ri_U^{-2} . This is possible because the mean velocity and density profiles do not relax to an invariant shape, but rather, the shoulders seen in figure 20 are increasingly accentuated with increasing Ri_U . This evolution can modify any scaling based on the assumption of self-preservation. This caveat applies to experimental results as well as to ODT, and may account for the absence of a unified picture of shear-driven entrainment (Fernando 1991).

As a practical matter, the high- Ri_U trend of the computed results implies entrainment rates below the experimental range for Ri_U greater than unity. As in other applications, ODT has some limitations, but may nevertheless prove useful for investigating interactions among multiple effects. For entrainment problems, there is a particular need to gain better understanding of flows involving combinations of shear, turbulent-diffusive, and buoyant forcings.

7. Discussion

One-dimensional turbulence (ODT) as formulated here is intended to identify the range of turbulence phenomena that can be captured with a minimal representation of the interplay of advection, viscosity, and buoyant forcing in turbulent flow. The essential elements of such a representation are identified as a mechanistically literal implementation of molecular-diffusive transport (requiring, at a minimum, one spatial coordinate), a stochastic advection process incorporating the essential ingredients of vortical motion (compressive strain and rotational folding), and a simple dimensionally based prescription of the ensemble of such motions. To incorporate these elements in a one-dimensional formulation, the triplet map, (2.1), is adopted as a one-dimensional representation of a turbulent eddy and the relation (2.14) is used to determine the eddy rate distribution as a function of the instantaneous profiles of streamwise velocity and density. Diverse phenomena are reproduced by integrating these elements into a numerical simulation in which the initial and boundary conditions corresponding to various turbulent flow configurations can be imposed.

It has been noted that adjustable parameters can be introduced into the large-eddy and small-eddy suppression mechanisms and the triplet-map definition. To maintain a focus on physical mechanisms rather than data fitting, these generalizations have not been implemented in the present, minimal formulation. The present formulation involves at most a single parameter that is determined either empirically or by applying a self-consistency condition, as appropriate for each application.

ODT may be viewed as a method of applying dimensional reasoning, in the spirit of mixing-length theory, to individual turbulent eddies rather than to ensemble-averaged properties. In this regard, a distinction can be drawn between mixing-length physics and mixing-length theory as conventionally applied. It has been shown here that mixing-length physics, as embodied in ODT, captures a variety of observed phenomena whose relation to mixing-length concepts is not self-evident. Notable among these are the sensitivity of the inertial-range spectral scaling to the nature of the large-scale forcing (§ 3.2.2), details of the structure of the turbulent kinetic energy balance near a wall (§ 4), non-classical heat-transfer scalings in Rayleigh convection (§ 5.2.2), the spatial structure of fluctuation properties of penetrative convection (§ 5.3), salient features of the Monin–Obukhov similarity functions (§ 6.1), and the dependence of shear-driven entrainment on stratification at low to moderate Ri (§ 6.3). Related results, presented elsewhere, include reproduction of observed non-classical scalings of buoyancy-driven flow between vertical walls, and reproduction of the observed dependence of the component flux ratio on the component density ratio at a turbulent double-diffusive interface.

The demonstration that ODT captures this variety of observed behaviours suggests that the manifestations of mixing-length physics in turbulence are significantly broader and deeper than heretofore supposed. The evidence presented here does not constitute a proof of this statement, but is substantial enough to indicate that this hypothesis merits further consideration.

ODT is particularly suited for simulation of molecular mixing in turbulence. The representation of molecular mixing in present-day turbulent-reacting-flow models is more rudimentary than the representation of advective transport. In this regard, ODT subsumes the demonstrated capabilities of the LEM, which has been applied successfully to otherwise intractable turbulent mixing problems (Kerstein & McMurtry 1994*b*; Kerstein, Cremer & McMurtry 1995). ODT extends LEM capabilities by incorporating two-way couplings between flow and scalar properties, such as buoyancy effects, that the LEM cannot capture.

Finally, the potential contribution of ODT to turbulence theory and analysis is considered. Like the LEM, ODT *per se* appears to be analytically intractable owing to the spatial non-locality of the advection process. (This non-locality has physically significant manifestations, e.g. admitting the possibility of countergradient transport.) Nevertheless, the LEM has spawned several analytical studies, including analysis of a simplified formulation (Holzer & Pumir 1993) and novel analytical approaches used to interpret LEM numerical results (Kerstein & McMurtry 1994*a,b*).

Analogous ties between ODT and theory can be envisioned. For example, Stull (1984) has formulated a one-dimensional non-local turbulent transport model applicable to geophysical flows. His evolution equation for mean properties is directly applicable to ODT. ODT simulations can therefore be used to estimate the turbulent exchange coefficients in his model and to test refinements and generalizations of his approach. More generally, ODT may broaden the analogy between random processes and microstructural properties of turbulence (Vainshtein *et al.* 1994).

The author would like to thank J. C. Kaimal, J. C. Klewicki, P. A. McMurtry and Z. Warhaft for helpful discussions. Special thanks are extended to Oscar P. Manley for encouraging this effort. The support provided by the Division of Engineering and Geosciences, Office of Basic Energy Sciences, US Department of Energy, is gratefully acknowledged.

Appendix A. Numerical implementation

A complete mathematical specification of ODT consists of

- (i) the mapping rule (2.1) with $f_1 = 1 - f_2 = \frac{1}{3}$;
- (ii) the stochastic process governing the eddy event sequence, based on the statistical hypotheses applied to the rate distribution (2.6) or its S-flow analogue (see below);
- (iii) large-eddy suppression to mitigate a large-scale anomaly;
- (iv) the viscous evolution equation (2.7) or (2.12) and any corresponding scalar equations, involving fluid properties ν and κ ;
- (v) small-eddy suppression; and
- (vi) the flow-dependent initial and boundary conditions for u and any advected scalars.

Here, some aspects of numerical implementation, including the extraction of statistical information from simulated realizations, are elaborated.

The one-dimensional domain $[0, Y]$ is discretized into cells of uniform size. The permutation rule (Kerstein 1991) for discrete implementation of the triplet map, (i), requires the number of cells comprising the mapping interval to be a multiple of 3, and no smaller than 6. This determines the smallest resolvable eddy size. The largest possible eddy size is the domain size Y . These constraints affect the discrete implementation of the eddy selection procedure, (ii), whose continuum formulation is outlined next.

For purposes of eddy selection, the allowed range of the nominal eddy location y_0 (namely, the lower terminus of the mapping interval) is the entire domain $[0, Y]$. If the upper terminus $y_0 + l$ exceeds Y , the mapping is not invoked except in simulations of homogeneous turbulence, in which periodic (or in some cases jump-periodic) boundary conditions are applied. (In all cases, l is not permitted to exceed Y .) For wall-bounded flows, this procedure confines eddies to the physical flow domain provided that walls are allowed only at $y = 0$ and Y . For the planar boundary layer, Y is assigned a value much larger than the layer thickness so that the omission of eddies extending beyond Y has negligible impact. No other provision is made for modification of the eddy space-time sequence owing to wall effects. Wall-flow structure is thus obtained solely by exclusion of eddies that violate physical confinement, in conjunction with the no-slip boundary condition applied to the viscous evolution equation.

Eddy selection can be implemented numerically by determining a total event rate and a joint p.d.f. of y_0 and l directly from (2.6). This procedure requires frequent reconstruction of the joint p.d.f., at prohibitive cost, so an equivalent but more efficient method is used. Specializing to T-flow, the event distribution during a given time interval Δt is expressed as

$$\lambda(l; y_0, t) \Delta t = P(l; y_0, t, \Delta t) f(l) g(y_0), \quad (\text{A } 1)$$

where $f(l)$ and $g(y_0)$ can be any desired p.d.f.s, and $P(l; y_0, t, \Delta t)$ is defined so that the appropriate ensemble of events is generated. Operationally, one pair of values (l, y_0) is chosen at each time step Δt by sampling from the p.d.f.s f and g . This identifies a candidate eddy, that may or may not be implemented. The implementation probability P is computed by substituting the chosen values of l and y_0 into (A 1) and using (2.6) to evaluate $\lambda(l; y_0, t)$. For any choices of f and g that include all allowed l and y_0 values, this procedure is equivalent to sampling the rate distribution λ in the limit of vanishing Δt . Sufficient numerical accuracy is obtained if Δt is small enough so that $P \ll 1$. This implies that the number of trials must greatly exceed the number of

events implemented. The method is nevertheless advantageous because costly p.d.f. reconstructions are avoided; at each time step, λ is evaluated for only one pair of values (l, y_0) .

The functional forms chosen for f and g do not affect the statistics of simulated realizations, but they may affect computational efficiency. Ideally, f and g should be chosen to minimize the variability of P , thereby maximizing the allowable Δt . In all reported computations, $g(y_0)$ is the uniform distribution over $[0, Y]$ and $f(l) = Bl^{-2}$ over the allowed range of l , where B is the p.d.f. normalization. These choices are not optimal, but they are found to be reasonably efficient for the flows simulated thus far. Adaptive time stepping within subdomains is implemented where advantageous.

For S-flow, eddy selection is implemented in the same manner, with the proviso that t is elapsed time in the Lagrangian sense, i.e. along the trajectories of individual fluid elements. The time increment corresponding to a given spatial increment dx is therefore $dt(y) = dx/u(y, x)$. dt is y dependent owing to the y dependence of streamwise velocity. The equivalent relation $d/dt = u d/dx$ yields the familiar evolution operator of boundary-layer equations. (See §2.3.1 for the S-flow formulation of viscous evolution.)

The eddy time scale can thus be expressed as an eddy streamwise increment $\chi(l; y_0, x) = u(\tilde{y}, x)\tau(l; y_0, x)$, where \tilde{y} is a nominal eddy location. The obvious choice is $\tilde{y} = y_0 + l/2$. The choice is inconsequential if l is less than the transverse distance over which u varies significantly. However, this does not hold in general, indicating that the relation between dt and dx cannot be implemented in an exact manner.

The spatial analogue of the eddy rate distribution is obtained by using χ in place of τ and substituting the definition of χ to obtain the eddy spatial distribution

$$\lambda(l; y_0, x) = A/[l^2 u(\tilde{y}, x)\tau(l; y_0, x)]. \quad (\text{A } 2)$$

The statistical hypotheses for this formulation are analogous to the T-flow statistical hypotheses.

The statistical hypotheses cause a large-scale anomaly, (iii), as follows. Consider the planar mixing layer with free-stream velocity difference Δ , with the initial velocity jump at $y = 0$ on the unbounded domain $(-\infty, \infty)$. The turbulent transport coefficient associated with eddies of size $l \gg L$, where L is the integral scale at time t , is of order $l^2/\tau(l; -l/2, t)$. This is of order $l\Delta$, diverging with increasing l .

In reality, transport due to eddies of size $l \gg L$ is negligible. In the model, as in turbulent flow, the characteristic time scale τ of eddies much larger than L exceeds the elapsed time t . Accordingly, the typical evolution of a simulated realization conforms to the usual shear flow growth laws. However, the statistical hypothesis allows the occasional occurrence of very large ($l \gg L$) events. These rare, unphysical events dominate the total transport, analogous to a previously noted artifact of the LEM (Kerstein 1991).

This artifact is more readily mitigated in ODT than in the LEM because in ODT, the instantaneous flow field is explicitly represented. For this purpose, (2.14) is modified by setting τ equal to ∞ (hence zero eddy rate) if the eddy interval contains more than a specified maximum fraction of laminar fluid. The fraction may be chosen empirically, but has arbitrarily been assigned the value $\frac{1}{2}$ in applications to date. Operationally, the laminar zone at time t consists of regions in which $u(y, t)$ is equal to its initial value $u(y, 0)$, within a small tolerance. (In DPE, this criterion is applied to ρ rather than u .) Computed results are found to be insensitive to the specified tolerance.

This large-eddy suppression mechanism is inoperative for homogeneous turbulence, which has no laminar outer flow. However, the smoothing effect of (2.5) at length scales

larger than the turbulence integral scale tends to mitigate the large-scale anomaly in homogeneous turbulence. Physically reasonable velocity statistics are obtained, but fluctuation properties of a passive scalar subject to an imposed gradient show excessive sensitivity to rare events, as noted in §3.2.4.

The only flow regimes considered here for which large-eddy suppression is operative are the spatially developing boundary layer (mentioned briefly in §4), penetrative convection (§5.3), and shear-driven entrainment (§6.3). For the latter two cases, the large-eddy suppression mechanism is non-essential owing to eddy suppression by the stable stratification of the laminar zone.

The key consideration in the numerical implementation of viscous evolution, (iv), is the effect of the concurrent advection process on the u profile. The advection process generates strong gradients and points of discontinuous du/dy , as illustrated in figure 1(b). Conventional finite-differencing is appropriate for solving (2.7), but numerical methods typically used for solving (2.12) are ineffective in this situation. To see why, consider the alternative S-flow formulation (2.9), (2.13). An Eulerian numerical method requires the streamwise increment Δx to be small enough so that the transverse displacement $v(y)\Delta x/u(y)$ is smaller than the u -profile fluctuation length scale. Owing to the integral on the right-hand side of (2.13), $v(y)$ at large y can be of a magnitude that requires exceedingly small Δx .

For present purposes, the following Lagrangian method is advantageous. The u profile is updated by solving (2.9) numerically in the fluid frame, i.e. with the transverse advection term vu_y omitted. The streamwise increment $(\Delta x)_u$ for this step is set by stability requirements, a less stringent criterion than the criterion determining Δx for the Eulerian method. The induced transverse velocity required to enforce continuity is computed by solving (2.13) with a coarser increment $(\Delta x)_v$. At each $(\Delta x)_v$ increment, a profile of displacements $v(y)(\Delta x)_v/u(y)$ determines a dilatation of the u profile, a costly but relatively infrequent operation. This operation can be infrequent because the only consideration determining $(\Delta x)_v$ is that the displacements should be small compared to the size of the turbulent zone.

In the numerical implementation, viscous evolution is invoked at increments $(\Delta x)_v$. At each increment, $(\Delta x)_v/(\Delta x)_u$ Lagrangian finite-difference steps are implemented based on (2.9) with vu_y omitted. Then a dilatation maps the Lagrangian update onto the Eulerian spatial domain. Domain decomposition with locally adaptive refinement of the streamwise increment is used for viscous as well as advective processes.

Small-eddy suppression, (v), is implemented by disallowing a mapping if its time scale τ is longer than the time scale $\tau_d = l^2/(16v)$ for viscous suppression of eddy motion. Here, τ_d is defined as the e-folding time for viscous dissipation of the turbulent kinetic energy within the mapping interval.

This definition is somewhat arbitrary. Inclusion of a free parameter would be appropriate, but the present objective is to minimize empiricism where possible. The development that follows is not a derivation of τ_d , but rather is a physically motivated basis for the selection of this quantity. Namely, τ_d is estimated by means of an analogy to the dissipation rate of $K_u = \langle u^2 \rangle / 2$ in ODT, which equals $v \langle (du'/dy)^2 \rangle$ (Appendix C). The local analogue of the quantity $\langle (du'/dy)^2 \rangle$ within the mapping interval is taken to be $(\Delta u/l)^2$. Based on the definition (2.4) of Δu , $\Delta u/2$ can be interpreted as the amplitude of a period- l sinusoidal component of the instantaneous u profile. The corresponding mean-square u fluctuation is $\frac{1}{2}(\Delta u/2)^2$. Therefore the local analogue of $\langle u^2 \rangle / 2$ is $(\Delta u)^2 / 16$.

According to the definition of τ_d that has been adopted, the dissipation rate of K_u is K_u/τ_d . Substituting local quantities in the expression for the dissipation rate of K_u , the relation $(\Delta u)^2/(16\tau_d) = v(\Delta u/l)^2$ is obtained, giving $\tau_d = l^2/(16v)$.

Boundary conditions, (vi), are applied in the usual manner in the viscous solution. They affect the advection process only through limitation of the physical domain in which eddies can be implemented, as mentioned earlier. Initial conditions are analogous to higher-dimensional formulations.

Statistics are gathered as from any unsteady flow simulation, except that transverse fluxes require special treatment owing to the implementation of transverse advection by means of an event sequence rather than a transverse velocity field. For example, the Reynolds stress $\langle u'v' \rangle$ in a T-flow is evaluated at given y by expressing it as the net transverse flux of u at y induced by turbulent advection. This is obtained from the simulation by summing the u values of domain cells that cross location y during each mapping event, with appropriate normalization; see Appendix C. (Each u value is multiplied by a sign corresponding to the flux direction.)

Appendix B. Three-dimensional interpretation of one-dimensional quantities

The relation between ODT properties and analogous properties of three-dimensional flow is based on the interpretation of the ODT profile $u(y, t)$ as a transverse profile of streamwise velocity. This interpretation is affected by differences between ODT conservation laws and those governing three-dimensional flow. For instance, ODT cannot redistribute kinetic energy among velocity components, as occurs in three-dimensional flow. Nevertheless, expressions for kinetic energy production and dissipation and other quantities of interest can be formulated that are at least roughly valid for the flows considered here.

In three-dimensional flow, the turbulent kinetic energy (per unit mass, assuming constant-density flow) is $q^2/2 = (u'^2 + v'^2 + w'^2)/2$, where u' , v' and w' are the deviations of the three velocity components from their ensemble-average values. In isotropic homogeneous turbulence, the average turbulent kinetic energy $K \equiv \langle q^2/2 \rangle$ is $\frac{3}{2}\langle u'^2 \rangle$. It is reasonable to interpret the quantity $\frac{3}{2}\langle u'^2 \rangle$ in ODT as the kinetic energy of isotropic homogeneous turbulence. (Henceforth, all discussion of energy refers to the average turbulent kinetic energy K .) Likewise, the ODT quantity

$$\epsilon_{\text{ODT}} = -\frac{3}{2}d\langle u'^2 \rangle/dt \quad (\text{B } 1)$$

can be interpreted as the model analogue of the energy dissipation rate $\epsilon = -dK/dt$.

In Appendix C, it is shown that the dissipation rate of $\langle u'^2 \rangle/2$ in ODT is equal to $v\langle (du'/dy)^2 \rangle$. From this and (B 1), the energy dissipation rate can be expressed as

$$\epsilon_{\text{ODT}} = 3v\langle (du'/dy)^2 \rangle \quad (\text{B } 2)$$

for isotropic homogeneous turbulence. This is the model analogue of the three-dimensional isotropic relation $\epsilon = \frac{15}{2}v\langle (du'/dy)^2 \rangle$ (Monin & Yaglom 1975). Owing to the different numerical coefficients in (B 2) and the three-dimensional relation, ODT cannot simultaneously match the three-dimensional energy dissipation rate and mean-square velocity cross-derivative. This artifact is due to the treatment of the u profile as a scalar from a mathematical viewpoint, evolving with no explicit coupling to other velocity components.

Different considerations apply to shear flows. Assume that the energy production is driven by the y variation of u , as is roughly valid for boundary-layer-type flows. In this case, the production of $\langle u'^2 \rangle/2$ within ODT approximates the energy production. In three-dimensional shear flow, this energy is redistributed among the three velocity components prior to its eventual dissipation, but in ODT, this energy remains in the

streamwise velocity component, owing to the conservation laws obeyed by the model. Therefore the dissipation rate of $\langle u^2 \rangle / 2$ within the model can be interpreted as the energy dissipation rate, i.e.

$$\epsilon_{\text{ODT}} = \nu \langle (du'/dy)^2 \rangle \quad (\text{B } 3)$$

for boundary-layer-type flows.

It is appealing to view model energetics as a self-contained representation of flow energetics and therefore apply (B 3) to isotropic turbulence as well, instead of adopting the kinematical picture that motivates (B 2). The lack of a unique, kinematically and dynamically consistent analogy between ODT and three-dimensional flow is an inherent limitation of the model. Here, (B 2) is applied to isotropic flows, though evidence favouring (B 3) is noted in § 3.1.3.

Consider now the production and dissipation of fluctuations θ' of a passive scalar θ . Three-dimensional scalar advection involves no redistribution of fluctuation intensity among vector components, so the ODT scalar fluctuation intensity $\theta'^2/2$ is analogous to $\theta^2/2$ in three-dimensional flow, whether homogeneous or boundary-layer like. The ODT balance equation for $\langle \theta'^2 \rangle / 2$ is formally equivalent to the balance equation for $\langle u^2 \rangle / 2$ (Appendix C), so the scalar dissipation rate $\epsilon_{\theta, \text{ODT}} \equiv -\frac{1}{2} d\langle \theta'^2 \rangle / dt$ can be expressed as

$$\epsilon_{\theta, \text{ODT}} = \kappa \langle (d\theta'/dy)^2 \rangle. \quad (\text{B } 4)$$

Here, the scalar dissipation rate is defined as the rate of change of $-\langle \theta'^2 \rangle / 2$ to emphasize the analogy between θ and u . (Some authors omit the factor $\frac{1}{2}$.) This analogy is more literal in ODT than in three-dimensional flow, because the profile $u(y, t)$ evolves as an advected scalar in ODT. Functionally, u is not a passive scalar because it determines the eddy rate distribution. Nevertheless, u is formally equivalent to a passive scalar because a passive scalar θ , with $Pr = 1$ and the same initial and boundary conditions as u , is subject to the same mapping events and the same molecular transport as u .

The ODT power spectrum of u , $E_{\text{ODT}}(k)$, is defined as the Fourier transform of the spatial autocorrelation $\langle u'(y)u'(y + \delta) \rangle$. With the normalization $\int_0^\infty E_{\text{ODT}}(k) dk = \langle u'^2 \rangle$, E_{ODT} is formally equivalent to the energy spectrum of transverse velocity fluctuations, conventionally denoted $E_2(k)$ (Hinze 1975). Here, spectra are considered solely in the context of incompressible isotropic flows. For such flows, E_2 is related to the commonly measured spectrum E_1 of longitudinal velocity fluctuations according to (Hinze 1975)

$$E_2 = \frac{1}{2} \left(E_1 - k \frac{\partial E_1}{\partial k} \right). \quad (\text{B } 5)$$

Although this is readily inverted to obtain $E_1(E_2)$, it is convenient to work with E_2 in order to avoid numerical issues related to the transformation of computed spectra. E_2 can also be expressed in terms of the three-dimensional spectrum E that is commonly used in theoretical analysis. The three-dimensional spectrum is not considered here. Henceforth, E denotes E_2 , or equivalently, E_{ODT} .

The ODT power spectrum of θ , $E_{\theta, \text{ODT}}(k)$, is defined as the Fourier transform of the spatial autocorrelation $\langle \theta'(y)\theta'(y + \delta) \rangle$. $E_{\theta, \text{ODT}}$ is formally equivalent to the one-dimensional scalar-fluctuation spectrum $E_{\theta 1}$ of three-dimensional flow, and can be transformed in the usual manner (Hinze 1975) to obtain the three-dimensional scalar-fluctuation spectrum E_θ . The normalization $\int_0^\infty E_{\theta, \text{ODT}}(k) dk = \langle \theta'^2 \rangle$, used by some but not all authors, is adopted. Henceforth, E_θ denotes $E_{\theta, \text{ODT}}$, or equivalently, $E_{\theta 1}$.

Many definitions of the turbulence integral scale L have been proposed. The

definitions used here are stated in the discussions of the individual flow configurations. For homogeneous turbulence, the commonly used definition

$$L = \langle u^2 \rangle^{3/2} / \epsilon \tag{B 6}$$

is adopted. For application to computed results, ϵ is evaluated using either of the equivalent relations (B 1) or (B 2).

Appendix C. Statistical properties of flow realizations

Model results are compared to measurements by averaging over ensembles of simulated flow realizations. For the purpose of formulating and interpreting these ensemble averages, it is useful to write a truncated form of the Navier–Stokes equation containing only those terms that are represented in some manner in ODT. Therefore consider the evolution equation

$$\frac{\partial u}{\partial t} + (\mathbf{W} \cdot \nabla)u = \nu \nabla_{\perp}^2 u \tag{C 1}$$

subject to the continuity constraint

$$\nabla \cdot \mathbf{W} = 0, \tag{C 2}$$

where \mathbf{W} denotes the vector (u, v) . Here, v represents the \perp -component of velocity, including vortical advection (represented by triplet maps in ODT) as well as the viscous contribution to v discussed in §2.3. Although these continuum equations cannot fully describe the evolution of a simulated ODT realization, it is shown that ODT realizations can be ensemble averaged to obtain quantities analogous to averages involving the quantity v in (C 1).

Indeed, v can be defined within individual realizations as well as in ensemble averages. To see this, (C 1) is transformed into an equation that is demonstrably obeyed by a simulated ODT realization. Specializing to Cartesian coordinates, (C 1) becomes

$$\frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = \nu \frac{\partial^2 u}{\partial y^2}. \tag{C 3}$$

As noted in § 2.1, ODT represents evolution either in t (for T-flow) or in x (for S-flow), so the first or second term of (C 3) may be dropped, depending on the flow type. Equation (C 3) formally corresponds to (2.9) specialized to the case of no streamwise pressure forcing for S-flow, and corresponds to the same specialization of (2.7) for T-flow, though as noted, v is now taken to include triplet-map advection. S-flow is considered for illustration, so the time derivative is dropped; the T-flow analogue of this analysis is straightforward.

For S-flow, (C 2) is used to write (C 3) in the form

$$\frac{\partial}{\partial x}(u^2) + \frac{\partial}{\partial y}(uv) = \nu \frac{\partial^2 u}{\partial y^2}. \tag{C 4}$$

Integration over a strip (y_0, ∞) in y , $(x, x + dx)$ in x gives

$$\int_{y_0}^{\infty} u^2(x + dx, y) dy - \int_{y_0}^{\infty} u^2(x, y) dy = u(x, y_0)v(x, y_0) dx - \nu \frac{\partial u(x, y_0)}{\partial y} dx \tag{C 5}$$

to leading order in dx , where terms evaluated at $y = \infty$ are assumed to vanish.

Formally, this is a conventional boundary-layer control-volume analysis (Kays &

Crawford 1980). It is reproduced here in order to highlight the physical significance of (C 5) in the present context. The left-hand side of (C 5) is the net transfer of streamwise momentum flux to the half-space $y > y_0$ within the streamwise interval $(x, x + dx)$. The last term is the corresponding viscous transfer of momentum flux. By subtraction, $u(x, y_0)v(x, y_0) dx$ must represent the only other momentum-flux transfer mechanism, advective transfer.

This deduction of the meaning of $u(x, y_0)v(x, y_0) dx$ demonstrates that no assumptions are necessary concerning the nature of the advection process. The term $u(x, y_0)v(x, y_0) dx$ is simply the net momentum-flux transfer by all mechanisms other than viscous gradient transport. In ODT, these mechanisms are advection by mapping events and the v -flow, (2.13), induced by viscous evolution.

The flow induced by viscous evolution is analogous to advective momentum-flux transfer in laminar flow. Namely, with the mappings omitted, implementation of ODT reduces to the solution of a conventional boundary-value problem for (C 4), and (C 5) has its conventional meaning. When mappings are introduced to represent turbulent advection, (C 4) no longer has a straightforward interpretation, but (C 5) remains valid provided that the mapping contribution is included in the advective transfer term.

To incorporate this contribution, the quantity $u(x, y_0)v(x, y_0) dx$ is evaluated for given x and y_0 in a simulated realization by monitoring momentum-flux transfers across y_0 , induced by (2.13) and by mapping events, in the streamwise interval $(x, x + dx)$. This data gathering is implemented in ODT simulations although $u(x, y_0)v(x, y_0) dx$ can alternatively be deduced by evaluating the other terms of (C 5). Advective-transfer monitoring serves to verify that simulated realizations satisfy momentum-flux balance to within the numerical accuracy of the algorithm. For higher-order balances, discussed shortly, the contribution of numerical dissipation is non-negligible. In this situation, indirect deduction of advective contributions would be unreliable.

The validity of this procedure is predicated on the fact that the triplet map, both in its continuum mathematical definition and in its discrete numerical implementation, is a measure-preserving map that advects fluid elements without changing properties of fluid elements. Were this not the case, mappings might modify integrands on the left-hand side of control-volume balances such as (C 5) in a manner that is not captured by the flux-monitoring procedure.

The foregoing analysis allows the model analogue of uw (and, by extension of this reasoning, $u^n v$ for $n \geq 0$) to be defined on a local, instantaneous basis, but it does not provide a physically sound representation of the instantaneous evolution of uw . For infinitesimal dx , there is an infinitesimal probability of mapping-induced transfer across y_0 in the interval $(x, x + dx)$. If such transfer does occur, a huge value of uw is implied. Thus, the streamwise evolution of uw in a given ODT realization does not mimic the evolution in continuum flow. In ODT, quantities like uw are 'generalized functions' (Lighthill 1970), physically meaningful only in the context of ensemble averages.

To form averages of interest, it is noted first that v is defined in ODT by control-volume analysis, analogous to (C 5), of the continuity equation (C 2). It is found that $v(x, y_0) dx$ corresponds to the advective transfer of volume flux (i.e. of u) across y_0 in the interval $(x, x + dx)$. Control-volume analysis of u^{n-1} times (C 4) likewise indicates that $u(x, y_0)^n v(x, y_0) dx$ corresponds to the advective transfer of u^{n+1} for $n > 0$. The quantity $\langle u^n v \rangle$ therefore corresponds to $1/(dx)$ times the ensemble average of the advective transfer of u^{n+1} across y_0 in the interval $(x, x + dx)$. For T-flow, analogous reasoning indicates that $\langle u^n v \rangle$ corresponds to $1/(dt)$ times the ensemble average of the advective transfer of u^n across y_0 during the time interval $(t, t + dt)$.

These relations allow the determination of averaged transverse fluxes such as the Reynolds-stress component $\langle u'v' \rangle$. (Here, the arguments x and y_0 of averaged variables are suppressed.) Where it arises in relations obtained by Reynolds averaging the Navier–Stokes equation, this quantity can be expressed in the form $\langle u'v' \rangle = \langle uv \rangle - \langle \langle u \rangle v \rangle - \langle u \langle v \rangle \rangle + \langle u \rangle \langle v \rangle = \langle uv \rangle - \langle u \rangle \langle v \rangle$. The intermediate expression is included here in order to indicate that this derivation does not carry over directly to ODT. In ODT, $\langle \psi v \rangle$ refers to an average of the advective transfer of the quantity ψ . The meaning of this averaging process is not obvious if ψ is itself an averaged quantity (e.g. $\langle u \rangle$) rather than a quantity that has an instantaneous definition.

Nevertheless, the decomposition $\langle u'v' \rangle = \langle uv \rangle - \langle u \rangle \langle v \rangle$ provides an operational definition of $\langle u'v' \rangle$ in terms of quantities that can be evaluated within ODT. As noted, the usual method for deriving relations of this type is not applicable within ODT. Therefore, when relations of this type are used to evaluate terms in an ODT balance equation, the validity of the resulting balance equation within ODT must be verified by control-volume analysis.

Analogous reasoning applies to the evaluation of scalar fluxes $\langle \theta'v' \rangle$. In fact, averages involving arbitrary powers of v can be evaluated by monitoring mapping-induced transfers of the v velocity, viewed as a cell property. In §2.4.1, the velocity attributed to a mapped cell is δ/τ , where δ is the mapping-induced cell displacement. The ensemble-average net rate of transfer of this quantity across y_0 can then be interpreted as the advective contribution to $\langle v^2 \rangle$. The method can be generalized to evaluate $\langle v^p \rangle$ for any $p > 1$ by monitoring transfers of the quantity $(\delta/\tau)^{p-1}$ by mapping events. Computed results for $\langle v'^2 \rangle$ are presented for several flows in §4, §5, and §6. For these flows, $\langle v \rangle = 0$, so $\langle v'^2 \rangle = \langle v^2 \rangle$.

The foregoing treatment of transverse fluxes allows the evaluation of all terms in higher-order balance equations based on (C 2) and (C 4). It has been noted that those equations imply control-volume balances such as (C 5) that are obeyed by ODT. The control-volume balances are general enough in their treatment of advection so that the terms of the balances can be defined operationally within ODT. The model is not governed by relations such as (C 2) and (C 4) *per se*, but such relations are useful shortcuts for deriving ODT balance equations by conventional methods (subject to verification by control-volume analysis).

For example, consider the balance of the u -component of turbulent kinetic energy, here denoted K_u . The derivation of the balance equation is entirely analogous to the conventional analysis (Hinze 1975) and therefore is omitted. In fact, ODT balances are simply subsets of the terms in conventional balances.

For S-flow, the ODT balance of $K_u = \langle u'^2 \rangle / 2$ is written in the form

$$C = P + T + V - D, \tag{C 6}$$

where the rates of convection, production, turbulent transport, viscous transport, and dissipation, respectively, are

$$C = \langle u \rangle \frac{\partial K_u}{\partial x} + \langle v \rangle \frac{\partial K_u}{\partial y},$$

$$P = -2K_u \frac{\partial \langle u \rangle}{\partial x} - \langle u'v' \rangle \frac{\partial \langle u \rangle}{\partial y}, \quad T = -\frac{1}{2} \frac{\partial}{\partial x} \langle u'^3 \rangle - \frac{1}{2} \frac{\partial}{\partial y} \langle u'^2 v' \rangle,$$

$$V = v \frac{\partial^2 K_u}{\partial y^2}, \quad D = v \left\langle \left(\frac{\partial u'}{\partial y} \right)^2 \right\rangle.$$

For T-flow, the convection term is replaced by $\partial K_u/\partial t$, and x -derivatives in the other terms are identically zero.

One consequence of (C 6) is the identification of the dissipation rate D of K_u , discussed in Appendix B. It was noted there that the production and dissipation of K_u in ODT should be interpreted as the production and dissipation of the total turbulent kinetic energy K in boundary-layer-type flows, owing to the conservation laws enforced in ODT. Therefore (C 6) is interpreted as the ODT analogue of the three-dimensional balance equation for K for purposes of comparing computed terms of (C 6) to measurements. On the other hand, computed profiles of $\langle u^2 \rangle^{1/2}$ are compared to measured streamwise velocity fluctuation profiles, owing to the kinematical interpretation of $u(y)$ as the streamwise velocity profile. These two interpretations cannot simultaneously be quantitatively accurate because the measured turbulent kinetic energy includes contributions from the v and w velocity components.

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